



## WASTE2ROAD

Biofuels from WASTE TO ROAD transport

LC-SC3-RES-21-2018 (818120)

### Deliverable Report

|                              |  |            |   |
|------------------------------|--|------------|---|
| <b>Deliverable ID</b>        | D7.4   |            |   |
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| <b>Lead beneficiary</b>      | VTT  |            |   |
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## Description of the deliverable content and purpose

The objective of WP 7 is to provide a robust mechanism for the dissemination and communication of the Waste2Road project activities and results. WP 7 will promote the Waste2Road project and results as widely and as efficiently as possible to all relevant stakeholders, scientific publications and media. A variety of platforms will be used to reach different stakeholders from public and private organizations, colleagues from related European projects, graduate students and the press. VTT and PDC will organize with the project partners two seminars for higher level students using Aspen Plus as a tool to evaluate and develop biogenic waste co-refining and involve in a workshop in the field of refinery processing, where results from these flow sheeting activities can be further exploited. The first biomass liquefaction modelling webinar was held in 22<sup>nd</sup> of April 2020 for higher-level university students together with the 4Refinery EU project at Aalto University in Finland. The second seminar was organized 20<sup>th</sup> of April 2021 for students around Europe. This deliverable D7.4 “Training seminar” highlights the content of webinars presentations that were presented by VTT, RESPOL, MOL, BTG, Aalborg University, PDC, CEA, TU Wien, Sintef, EGE and BTG Bioliquids.

The deliverable D7.4 will be submitted twice during the project period, at M24 and at M42. This deliverable is a second version, including the results from both the first and second seminar.

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## 1 Introduction

Biomass liquefaction modelling webinars were held on 22<sup>nd</sup> of April 2020 and 20<sup>th</sup> of April 2021 for higher-level university students. Webinar presentations covered several aspects of modelling biomass in fast pyrolysis and hydrothermal liquefaction processes. Different experiences in co-processing of bio-crudes in refineries have been presented as well. The first webinar was held basically for the chemical engineering and plant design students at Aalto University, but the event was also open for other people from the industry. The second seminar was organized for students around Europe. The webinars were very successful with approximately 40-50 participants in each seminar. Appendix contains some slides that were presented in the webinars.

## 2 Webinar program

Both webinars were focusing on the production of biocrudes by fast pyrolysis and HTL and co-processing the biocrudes in the oil refinery. The first seminar contained also a modelling exercise for the students. The agenda for the seminars are presented in Table 1 and Table 2.

*Table 1. Agenda for the first student seminar.*

|             |   |
|-------------|---|
| 8:30-8:45   | Logging into the webinar  |
| 8:45-9:00   | Introduction to the topic of the webinar<br>Kristian Melin, VTT<br>Pekka Oinas, Aalto University  |
| 9:00-9:30   | Latest developments in pyrolysis and upgrading  |
| 9:30-10:00  | Latest developments and activities in co-processing biocrudes by FCC and other technologies<br>Rebeca Yuste Pilar, Repsol, Spain                                |
| 10:00-10:30 | Co-hydrotreatment of bio-crudes. Pilot plant experiment and engineering consideration.<br>László Leveles, MOL Refining R&D                                      |
| 10:30-10:40 | Break   |
| 10:40-11:10 | Modelling of fast pyrolysis with COCO freeware software case Empyro fast pyrolysis plant.<br>Robbie Venderbosch, BTG, The Netherlands                           |
| 11:10-11:40 | Modelling hydrothermal liquefaction processes.<br>Thomas Pederson Aalborg University, Denmark   |
| 11:40-12:10 | Modelling of biocrude upgrading including stabilization and hydrodeoxygenation with aspen and empirical modelling of co-FCC using MODDE.<br>Kristian Melin, VTT |
| 12:10-12:40 | Techno-economic assessment of conceptual processes and life cycle costing.<br>Mieke Nieder-Heitmann, Process Design Center, The Netherlands                     |
| 12:40-13:15 | Break   |
| 13:15-13:30 | Introduction to Modelling exercise with Aspen Plus to modelling fast pyrolysis of the Empyro Plan in the Netherlands  |
| 13:30-15:00 | Individual work for students  |
| 15:15-15:45 | Demo of the modelling exercise and showing the correct results  |
| 15:45-15:50 | Final words and end of the webinar  |

Table 2. Agenda for the second student seminar.

|             |   |
|-------------|---|
| 8:30-8:45   | Logging in to the seminar   |
| 8:45-9:00   | Introduction to the topic of the webinar<br>Christian Lindfors, VTT Technical Research Centre of Finland  |
| 9:00-9:30   | Fast pyrolysis of waste materials<br>Christian Lindfors, VTT, Finland   |
| 9:30-10:00  | HTL operation with waste materials<br>Anne Roubaud, French Alternative Energies and Atomic Energy Commission (CEA), France                      |
| 10:00-10:30 | Co-processing of biogenic feedstocks in an FCC pilot plant<br>Helene Lutz TU Wien, Austria  |
| 10:30-10:40 | Break   |
| 10:40-11:10 | Co-hydroprocessing of bio-oil to obtain diesel middle distillates fuels<br>Rune Lødeng Sintef, Norway   |
| 11:10-11:40 | Stabilization of bio-oil and modelling of fast pyrolysis using COCO software<br>Robbie Venderbosch, Biomass Technology Group (BTG), Netherlands |
| 11:40-12:10 | Modelling hydrothermal liquefaction process<br>Thomas Helmer Pedersen, Aalborg University, Denmark  |
| 12:10-12:20 | Break   |
| 12:20-12:50 | Techno-economic assessment of conceptual processes and life cycle costing<br>Mieke Nieder-Heitmann, Process Design Center, Netherlands          |
| 12:50-13:20 | Where is the energy in the city waste?<br>Johnny Stuen, Oslo Kommune Energigjenvinningsetaten (EGE), Norway                                     |
| 13:20-14:00 | Commercialization activities about pyrolysis<br>Gerhard Muggen, BTG Bioliquids, Netherlands   |
| 14:00-14:05 | Final words and end of the seminar  |

### 3 Webinar key learning points

Fast pyrolysis and HTL are promising technologies to convert solid biomass into an intermediate biocrude. The commercial plants in operation are using clean feedstock, but in future target is to use more waste based material. This will have a big impact not only on the primary liquefaction process, but also on the downstream upgrading processes, which are very sensitive to high metal, sulphur and chlorine contents in the biocrude.

Integration of bio-liquids in a refinery was discussed thoroughly in the webinars. Complexity of bio-crude composition was highlighted by presenting comparative overall properties of bio-liquids produced by pyrolysis and hydrothermal liquefaction. Several co-feeding points in a refinery were discussed and justified.

REPSOL, MOL, Sintef and TU Wien shared their experiences in Fluid catalytic cracking and co-hydrotreatment, respectively.

BTG and BTG Bioliquids presented the status of pyrolysis as a mature and cheap process that has great potentials especially when integrated into refineries. Furthermore, a presentation was dedicated to

explain how to use COCO to model a pyrolysis process; COCO is a free modeling tool that students can use for modelling different processes.

Modelling of hydrothermal liquefaction process was introduced by Aalborg University. Presentation focused on non-conventional solid approach in biomass modelling using Aspen plus. Some related calculations were highlighted as well. In addition, integration of hydrothermal liquefaction process in a refinery has been presented as a case study.

VTT presented Aspen plus as a modelling tool to find a suitable co-processing route. Modelling based on chemical composition, distillation curve or creating an empirical model were methodically explained in the presentation.

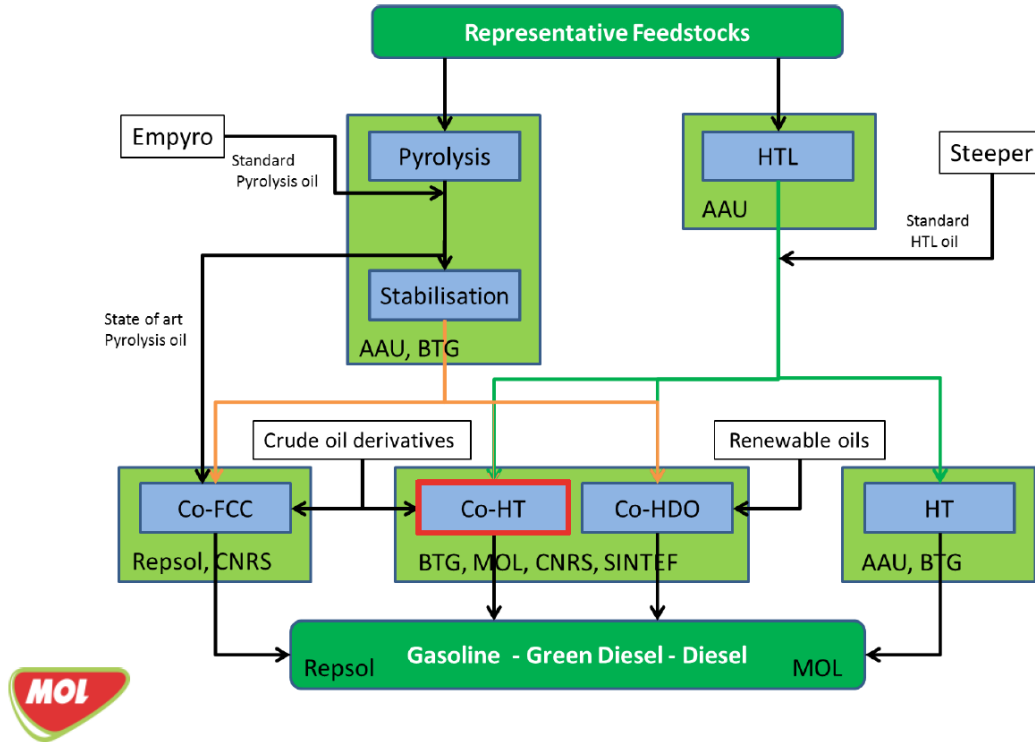
In addition to that, PDC presented detailed techno-economical assessment and life cycle costing calculations. Economic parameters such as production cost, IRR and NPV were used to present techno-economical assessment results.

The webinar ended with a modelling exercise for students to practice using Aspen plus. Simplified simulation model was introduced to simulate the fast pyrolysis process in Empyro plant. In the exercise, biomass and pyrolysis products were modelled by using the non-conventional approach and by utilizing a yield reactor with already defined products, respectively.

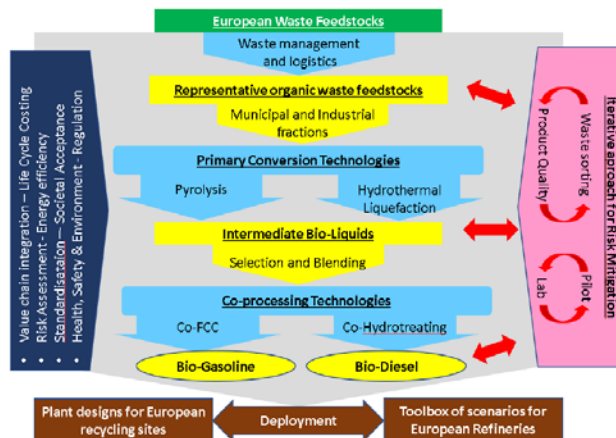
## 4 Appendix



### 4Refinery concept



### WASTE2ROAD concept



WASTE2ROAD project aims to develop a **new generation of cost-effective biofuels** from a selected range of **low cost and abundant biogenic residues and waste fractions**, aiming to achieve **high overall carbon yields > 45%** while reducing **greenhouse gases emissions (GHG) by > 80%** compared to fossil fuels.

The consortium covers the full value chain from waste collection and recycling, to bio-conversion (liquefaction) and co-refining, through to validation of the biofuels for the use of road transport.

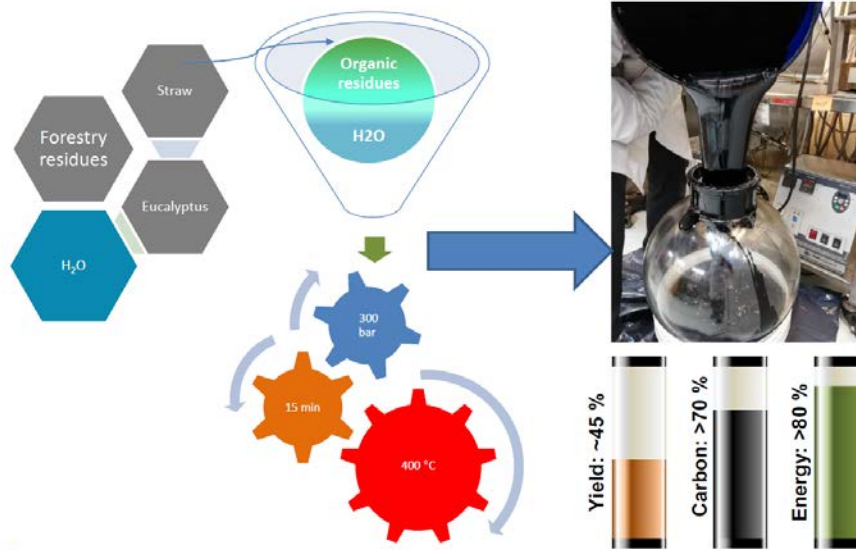
The project aims to achieve pilot testing at TRL 5.



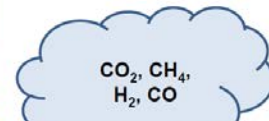
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### What is HTL – the simple version



### 4refinery



Gas production



Char & nutrients

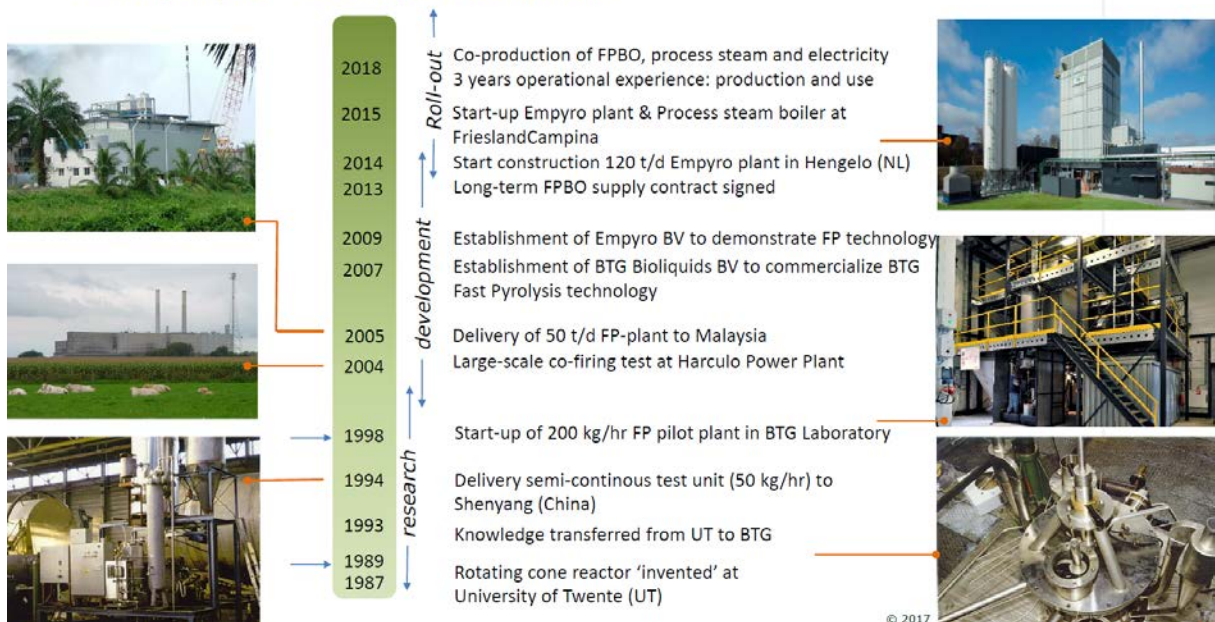
Mimics the natural process for crude oil production.

Time reduction: 100 mio. yrs vs. 15 min!



4refinery - Scenarios for integration of bio-liquids in existing REFINERY processes  
European Union's Horizon 2020 research and innovation programme, GA No. 727531

### Fast Pyrolysis – development timeline





## Integration of bio-liquids in refinery

### Potential options of integration

Three possible insertion points of bio-liquids in a refinery:

- (1) By converting bio-liquids in stand-alone units into a crude that can be co-processed with conventional crude oil.
- (2) **Upgrading bio-liquids into refinery-ready intermediates that are compatible with refinery streams.**
- (3) Upgrading the liquids in stand-alone units into finished/near-finished blend stock that will be minimally processed at the refinery (drop-in fuels).

4REFINERY

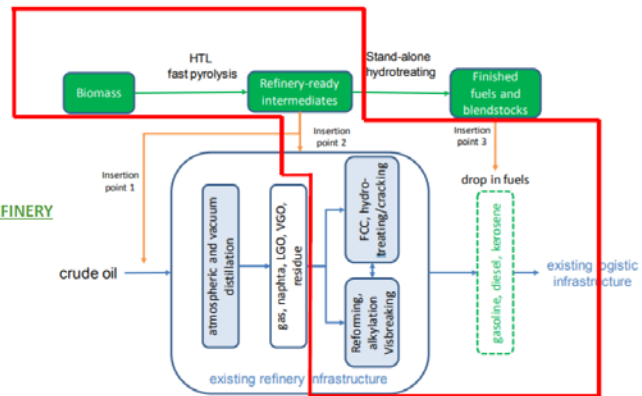


Figure 10: Insertion points for bio-liquids, biofuel intermediates, or finished hydrocarbon biofuels to integrate into existing petroleum refineries and distribution infrastructure.



4refinery - Scenarios FOR integration of bio-liquids in existing REFINERY processes  
European Union's Horizon 2020 research and innovation program, GA No. 727531

## Chemical, physical and technical challenges in processing of renewables

- **High oxygen content;** Exothermic reactions and a high consumption of hydrogen
  - Might include a high H<sub>2</sub>O content
- **Materials;** The risk of corrosion due to a high acid number, a high chlorine content and the presence of oxygenated compounds, carboxylic acids
- **Contaminants;** Deposits causing pressure drop and catalyst deactivation due to the presence of components such as Si and P, and others
- **Product Quality;** The establish on the density and cold flow properties of the end product,
- **Feedstock supply;** The ability to secure a reliable supply of renewable feedstocks of sufficient quality

**W2R solution is diversity in feedstock types and technology**

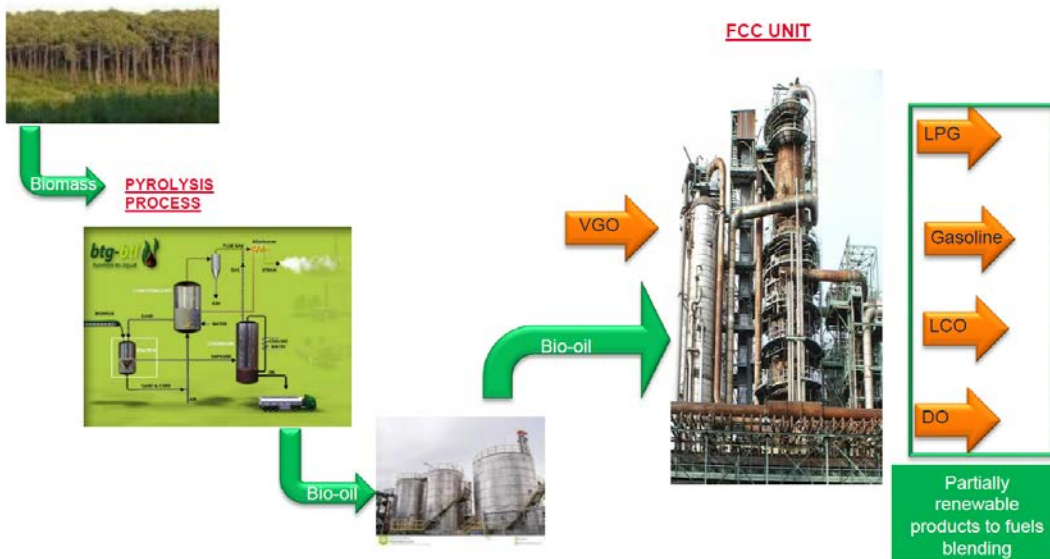


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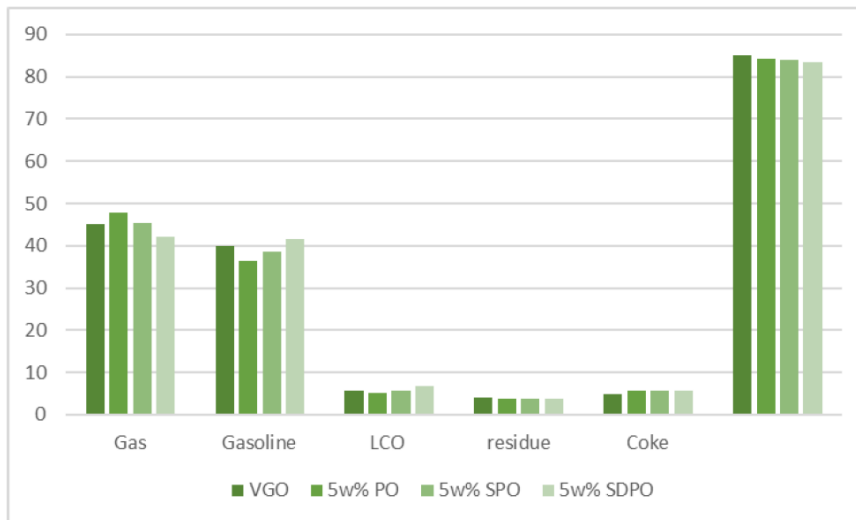


### 3. Co-processing of bio-feedstocks in FCC

*Utilize existing refinery infrastructure*



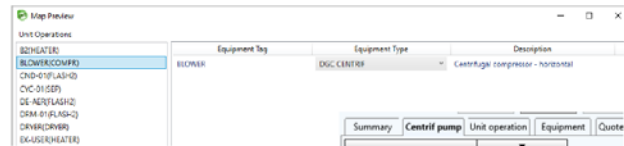
Vienna University of Technology - Institute of Chemical Engineering  
Fluidized Bed Systems & Refinery Technology



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## Aspen Process Economic Analyzer

- Used in many research articles
- How to use it:
  - Map equipment
  - Size
  - Evaluate & Analyze
  - Adjust for material of construction
- Always ‘sanity-check’ each unit of equipment since some equipment unit costs may not be accurate
  - Not calculated due to an error, or
  - If it is a batch unit or the residence time is specific, the cost needs to be adjusted
  - For example: batch processes, adsorption columns, and most likely some new equipment units specific to bio-processing
  - Think about the year of the costing (e.g. Aspen Plus v8.6 is 2016) and adjust for time value if required



| Summary                     | Centrif pump | Unit operation      | Equipment | Quote |
|-----------------------------|--------------|---------------------|-----------|-------|
| User tag number             |              | PLMP-1-IP           |           |       |
| Remarks 1                   |              | Equipment mapped    |           |       |
| Quoted cost per item (USD)  |              |                     |           |       |
| Currency unit for matt cost |              |                     |           |       |
| Number of identical items   |              |                     |           |       |
| <b>Installation option</b>  |              |                     |           |       |
| Casing material             |              |                     |           |       |
| Liquid flow rate (cum/hr)   | CS           | Carbon steel        |           |       |
| Fluid head (meter)          | CI           | Cast iron           |           |       |
| Fluid head (meter)          | A 204        | Low alloy, grade C  |           |       |
| Speed (rpm)                 | AS338        | Low alloy, grade 1B |           |       |
| Fluid specific gravity      | SS           | Stainless steel     |           |       |
| Driver power (KW)           | SS304        | SS304               |           |       |
|                             | SS116        | SS116               |           |       |



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