



HTL operation with waste materials

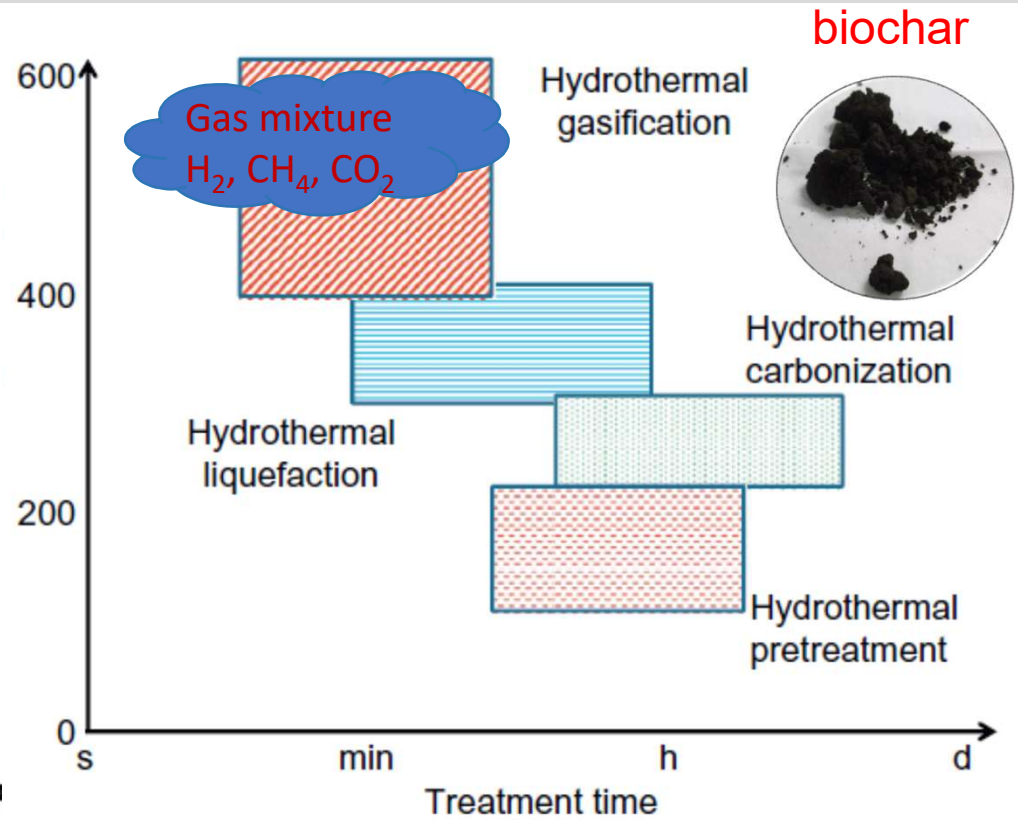
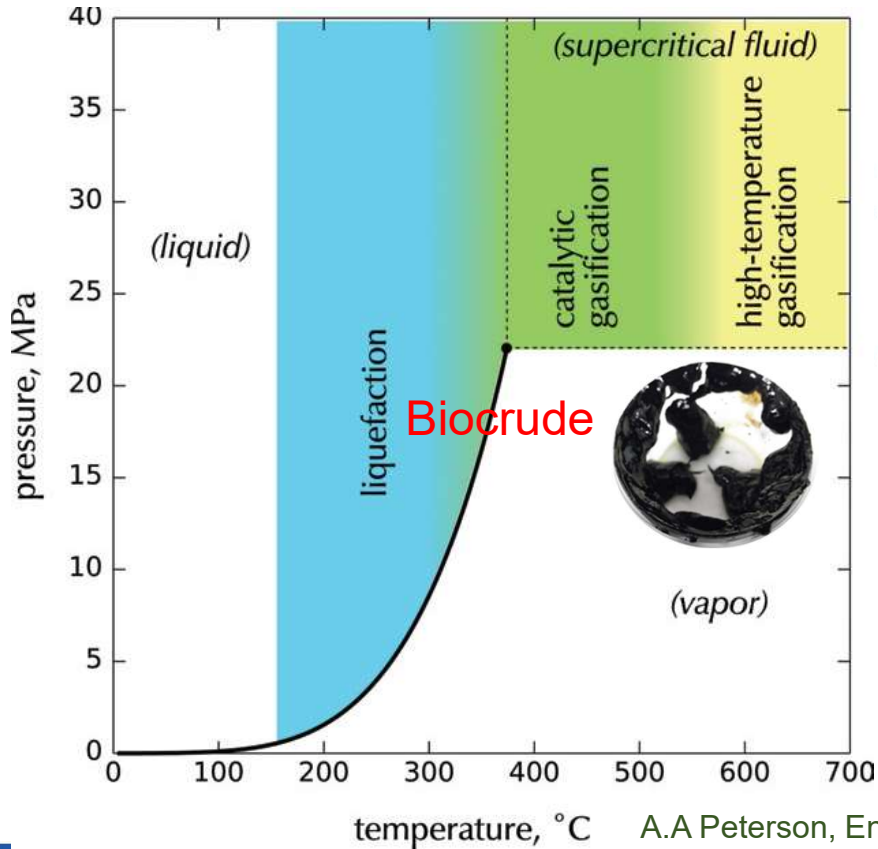
Anne Roubaud
CEA LITEN

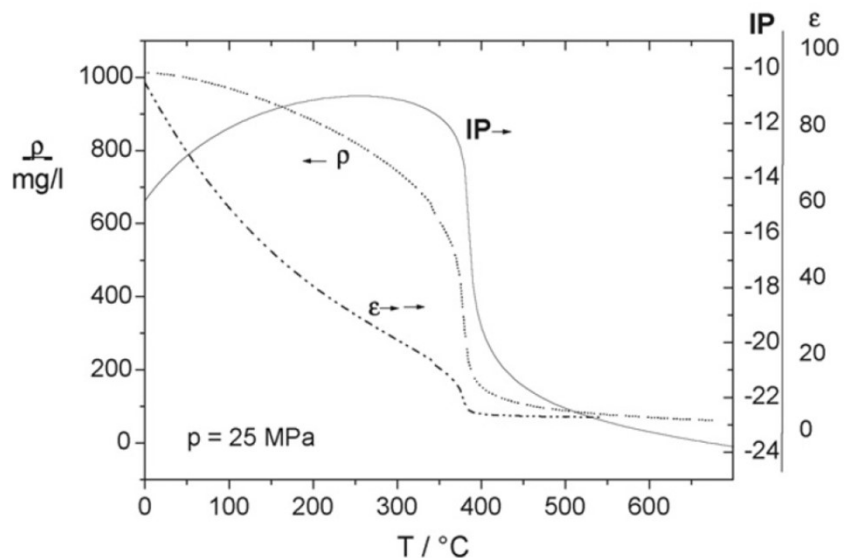
20/04/2021



This project has received funding from the European Union's Horizon 2020 research and innovation programme under grant agreement No 818120.

HYDROTHERMAL PROCESSES





A. Kruse, E. Dinjus / *J. of Supercritical Fluids* 39 (2007) 362–380

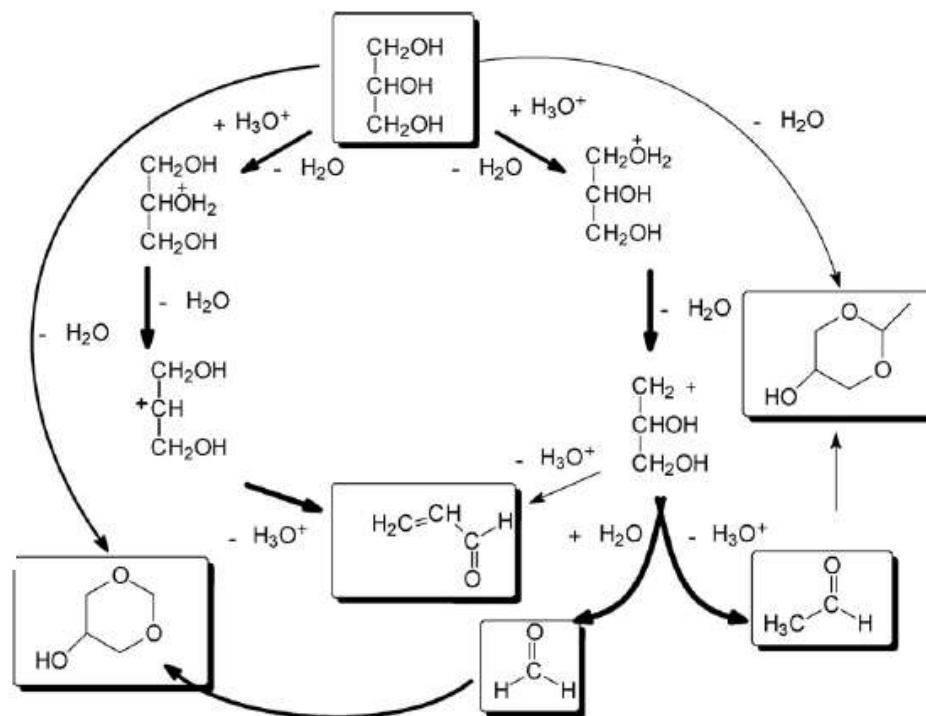


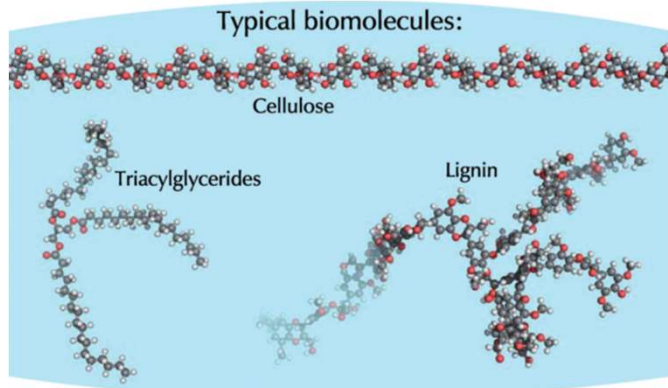
Fig. 9. Main reaction pathways of the ionic reaction mechanism, calculated for 45 MPa, 350°C and 118 s.

A. Kruse, E. Dinjus / *J. of Supercritical Fluids* 41 (2007) 361–379



HTL OF BIOMASS

biomass

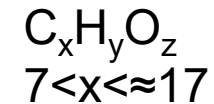


Hydrothermal Liquefaction

H_2O ~200-380°C / ~7-30MPa



Biocrude



Dehydration -H₂O

Deamination -NH₂

Decarboxylation -CO₂

	Hydrothermal liquefaction	Fast pyrolysis
Moisture (wt%)	5	25
Elemental analysis (dry basis, wt%)		
C	77	58
H	8	6
O	12	36
Heating content (MJ kg ⁻¹)	35.7	22.6
Viscosity (cps)	15 000 @ 61 °C	59 @ 40 °C

- A lower oxygen and nitrogen content
- Need of upgrading for drop-in application (O% < 1%, viscosity)

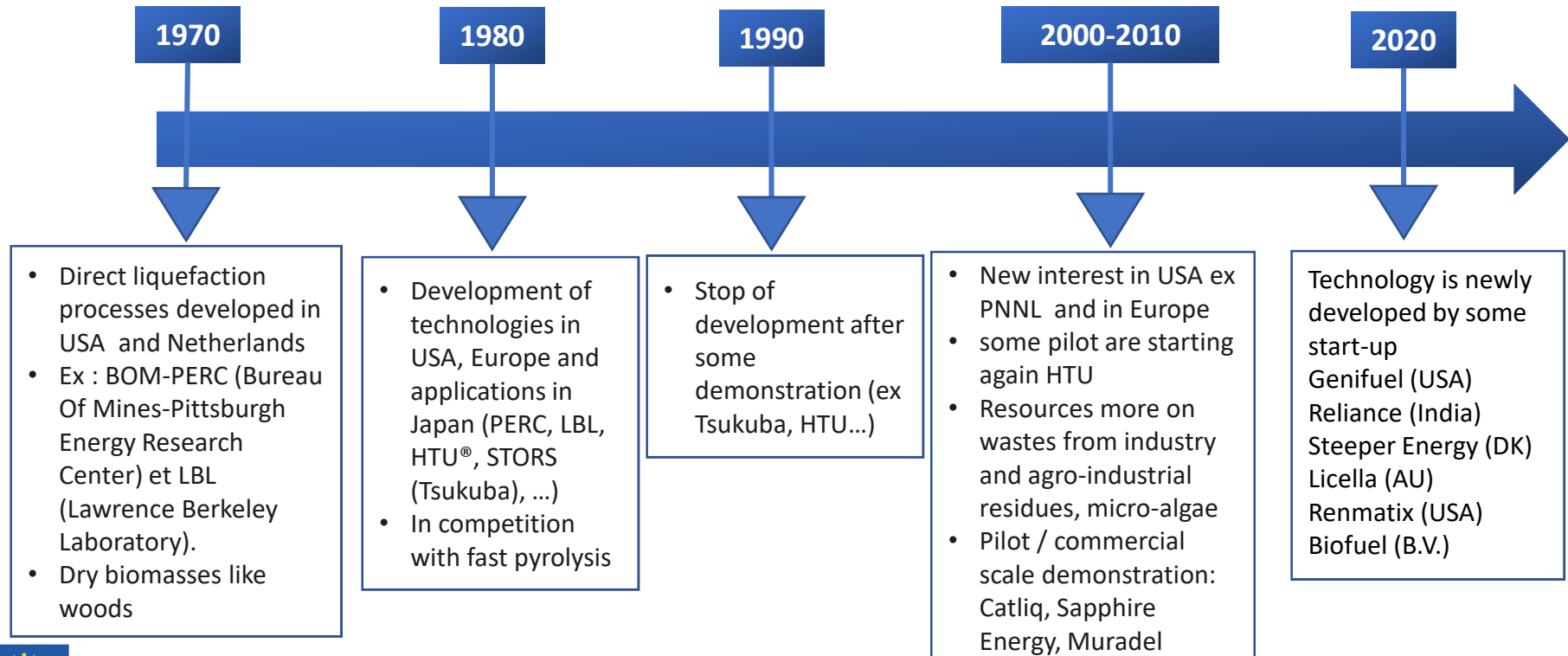
Ref :A.A Peterson, Energy Environ. Sci., 2008, 1, 32–65

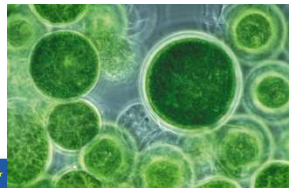


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Fossil fuel crisis

Cheap crude oil





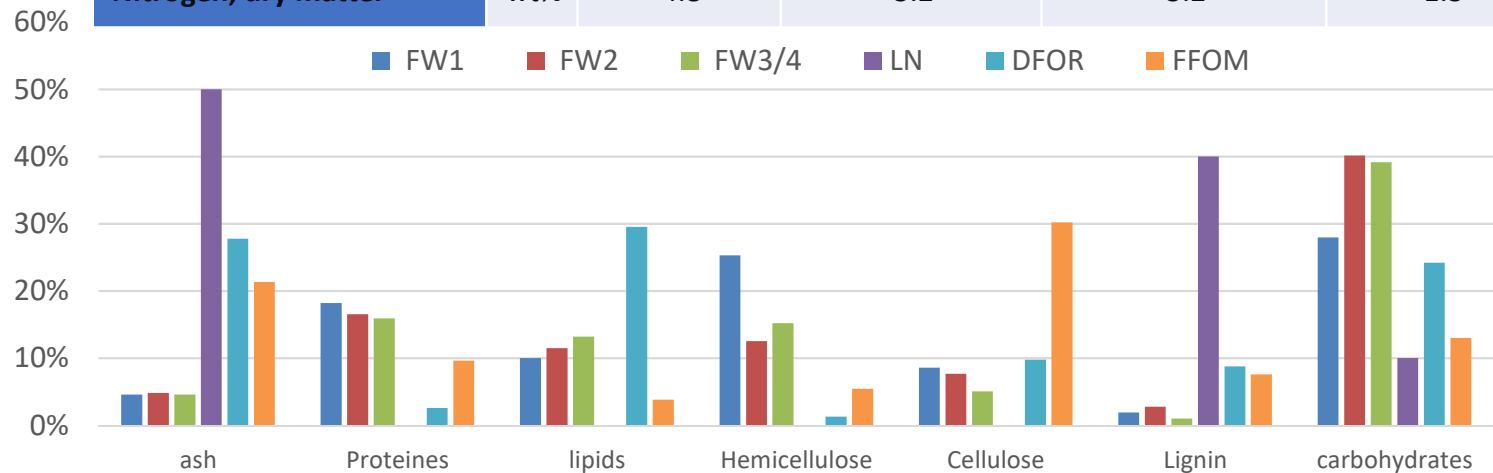
- HTL => wet wastes (RH > 50%w)
- Wet wastes and wet biomasses
Food wastes, sewage sludge, organic fraction of municipal solid wastes, agro-industrial residues, black liquor from pulp&paper industry, micro-algae, whey, vinasse...
- Conversion of the organic fraction
- Inorganics can have a catalytic effect
- Will be mainly recovered in the char fraction
- Toxics elements in => toxics elements out



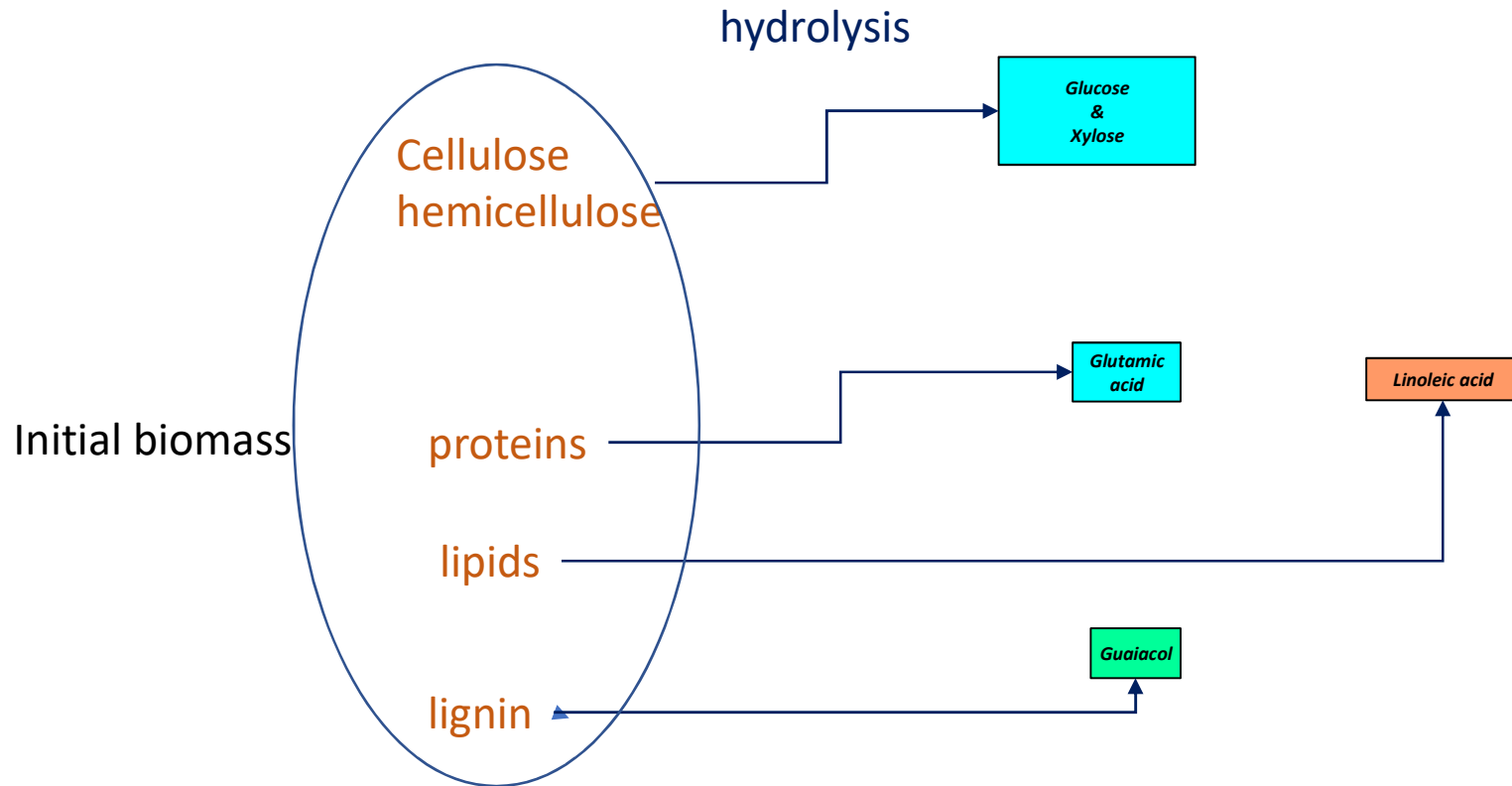
WASTE COMPOSITION

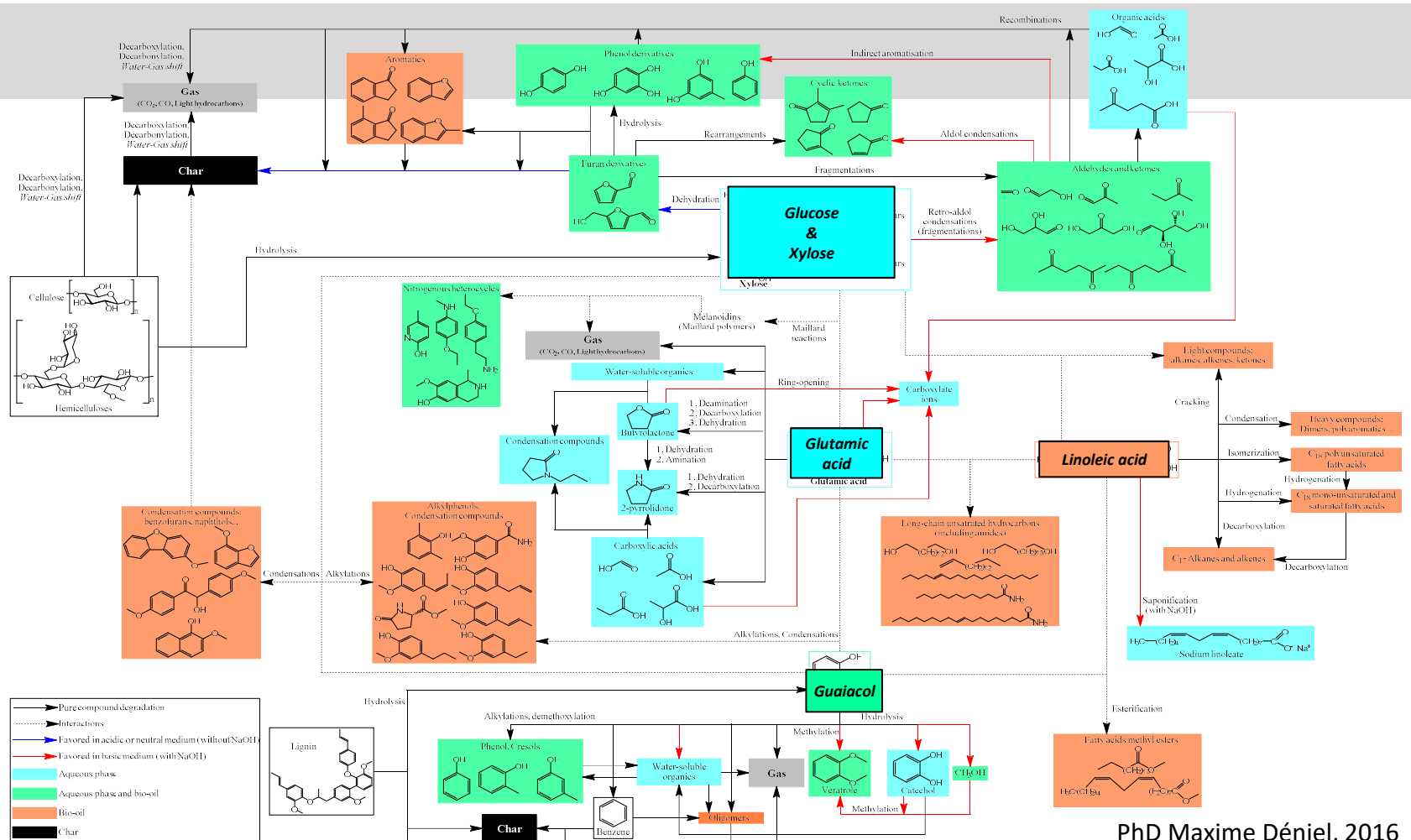


		Digestate	Food waste 1	Food waste 2	Black liquor
Feedstock origin		EGE	CEA Restaurant	CEA Restaurant	Grenoble INP
Total moisture, as received	wt%	42	90	82	86.0
Ash 550 °C, dry matter	wt%	28.0	5.1	4.9	50
Carbon , dry matter	wt%	37.6	47.3	43.8	32.8
Hydrogen, dry matter	wt%	5.9	6.3	8.1	55.2
Nitrogen, dry matter	wt%	4.8	3.2	3.2	1.3



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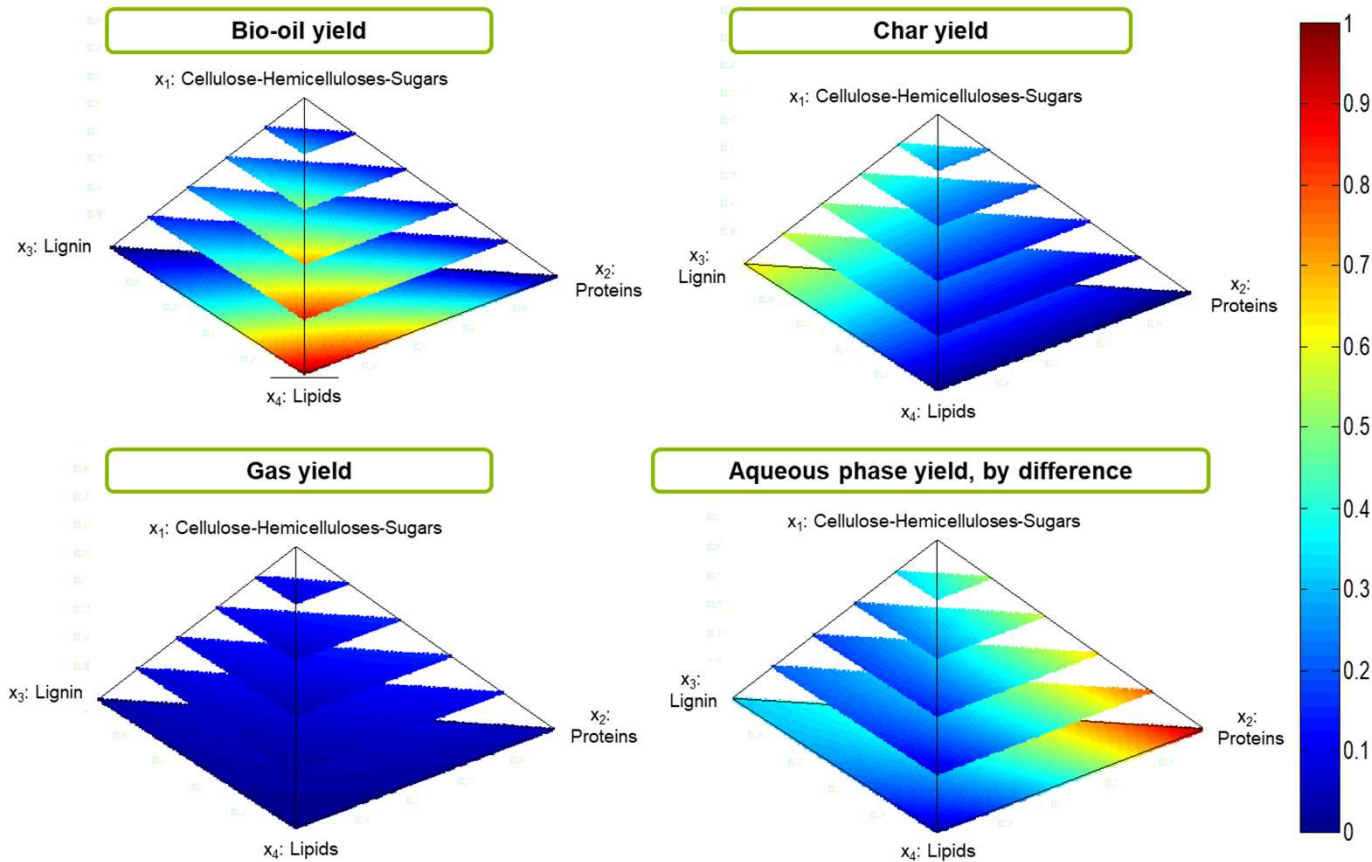


PhD Maxime Déniel, 2016



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PREDICTION OF CONVERSION YIELDS



Quadratic regression

$$y = \sum_{i=1}^4 b_i x_i + \sum_{i<j}^4 b_{ij} x_i x_j$$

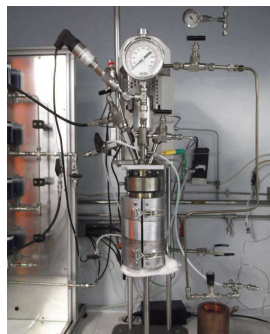
PhD Maxime Déniel,
2016



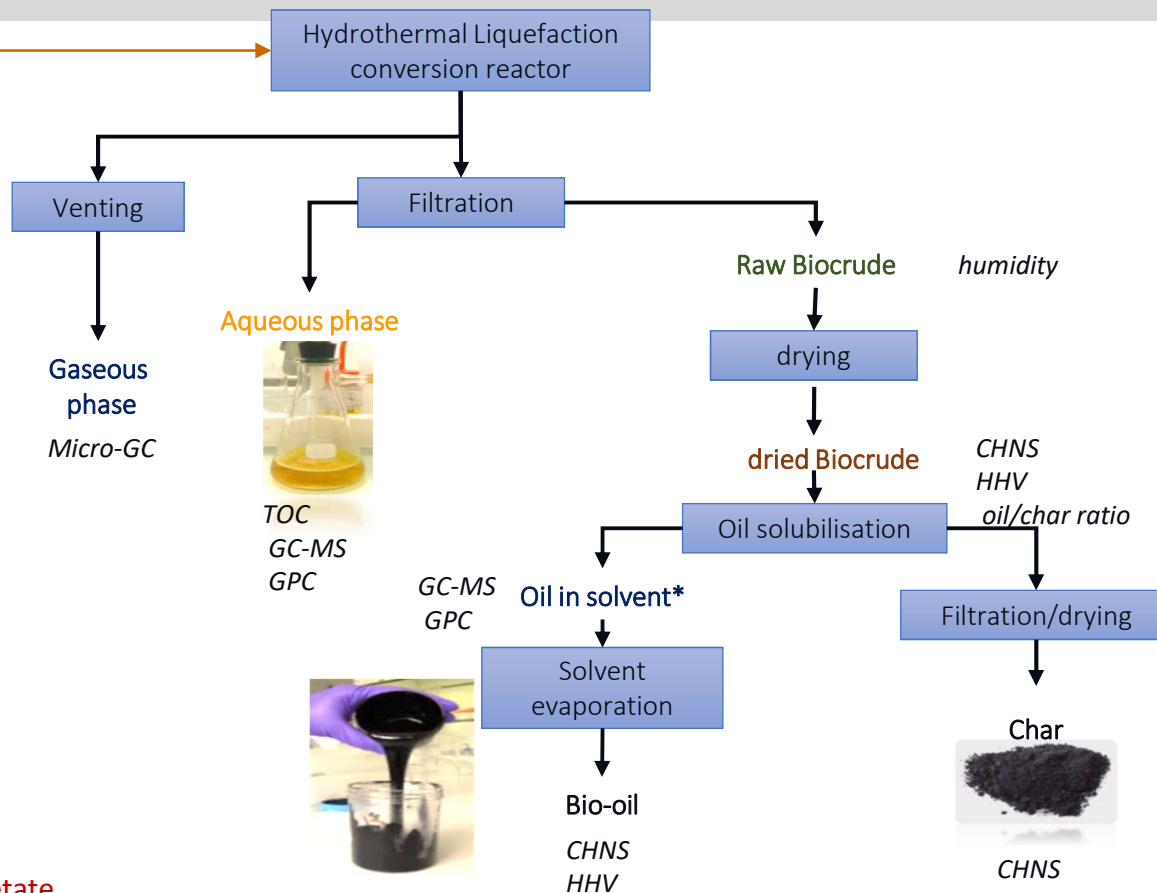
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ANALYTICAL PROCEDURE

Biomass mixture
10 %w dm in water



Batch reactor
600 mL
RT=30 min
Heat-up rate 15°C/min
Autogenous pressure
300°C, P>90 bar

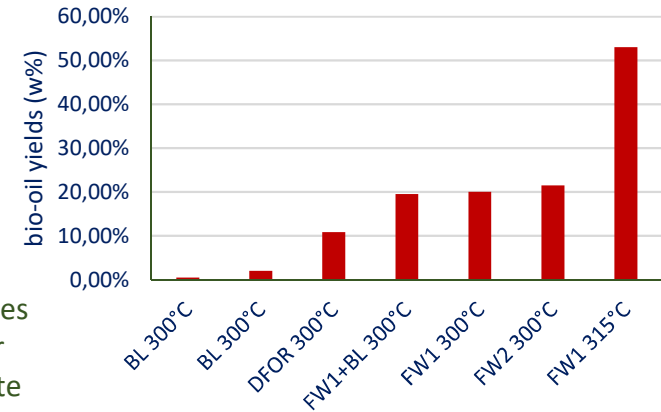
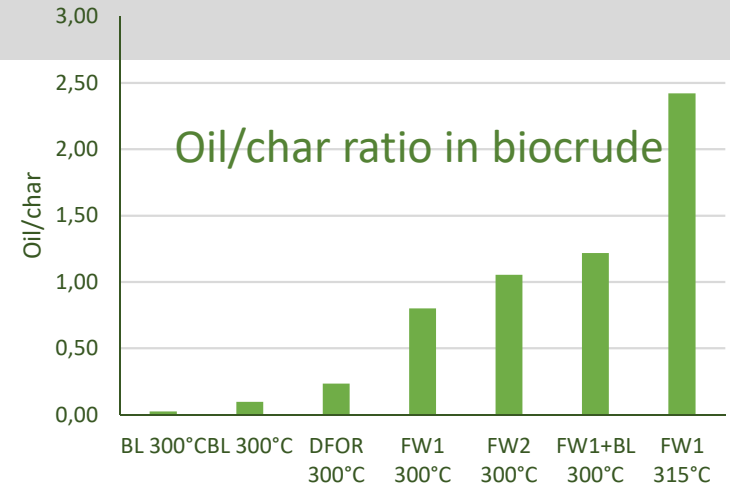
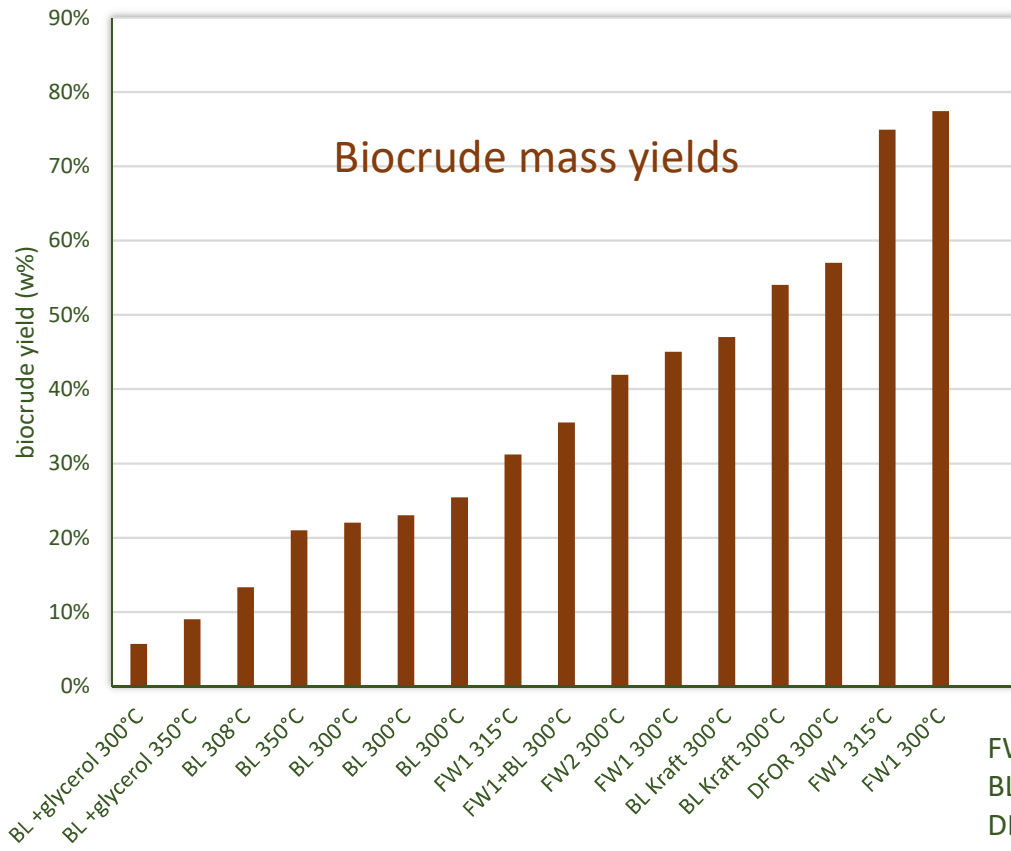


*Solvent = ethyl acetate



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SCREENING OF RESOURCES in batch

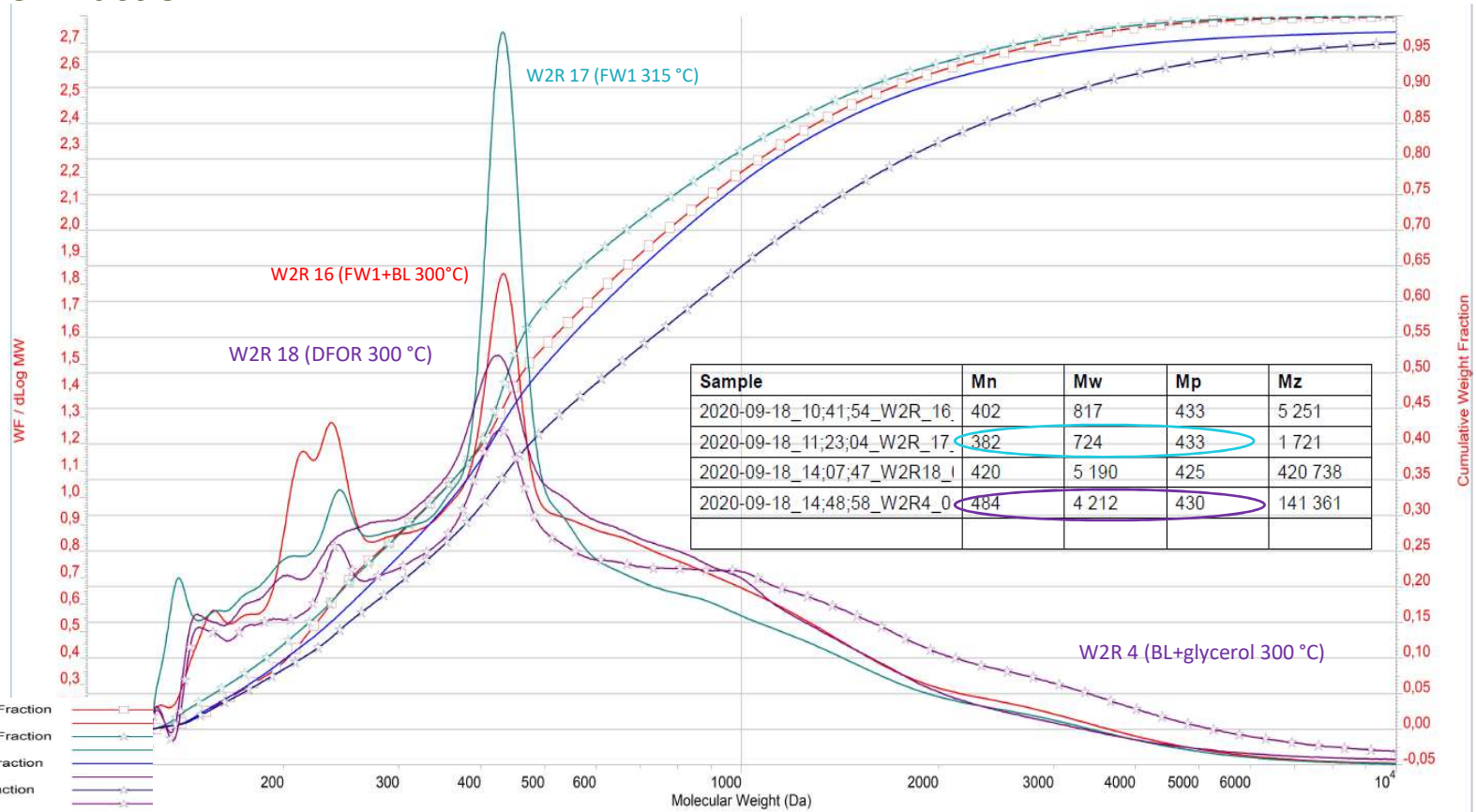


FW= food wastes
BL=black liquor
DFOR= digestate



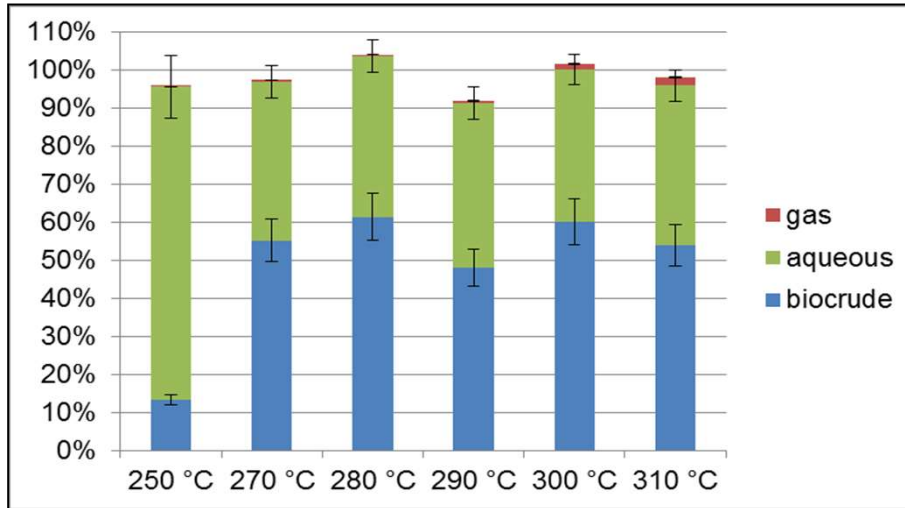
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GPC analysis of oil fraction in THF



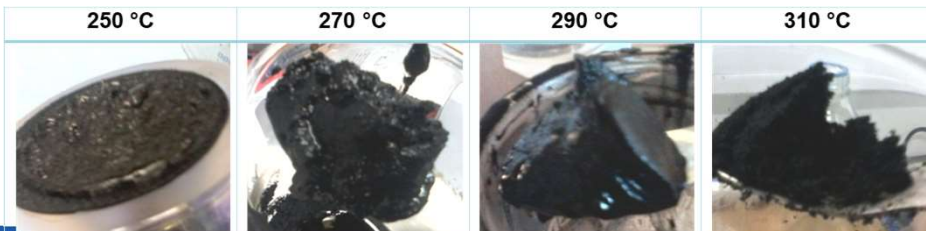
W2R_16_01-0001.vdx : Cumulative Weight Fraction
 W2R_16_01-0001.vdx : WF / dLog MW
 W2R_17_01-0001.vdx : Cumulative Weight Fraction
 W2R_17_01-0001.vdx : WF / dLog MW
 W2R18_01-0001.vdx : Cumulative Weight Fraction
 W2R18_01-0001.vdx : WF / dLog MW
 W2R4_01-0001.vdx : Cumulative Weight Fraction
 W2R4_01-0001.vdx : WF / dLog MW

EXAMPLE OF RESULTS WITH BLACK LIQUOR



Carbon distribution in %C

At 280-300 °C : 60% of C ended up in the biocrude and 40% in the aqueous phase
Gas production is marginal, mainly CO₂

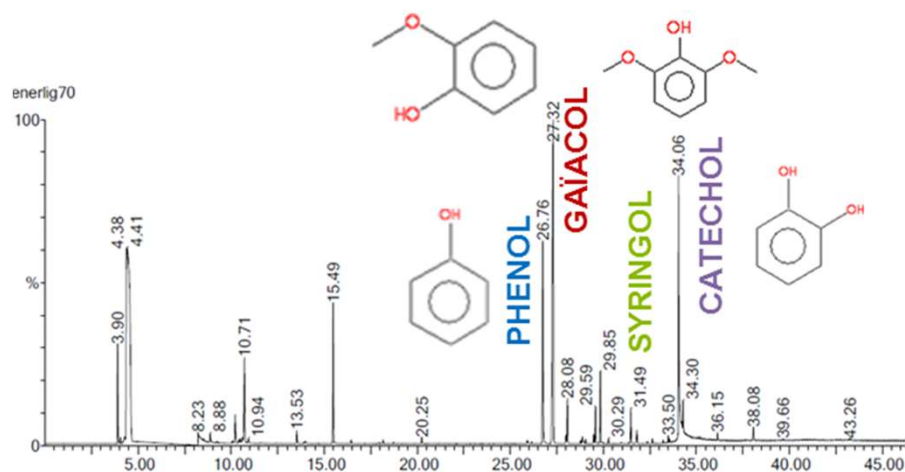


PhD Marion Huet, 2015

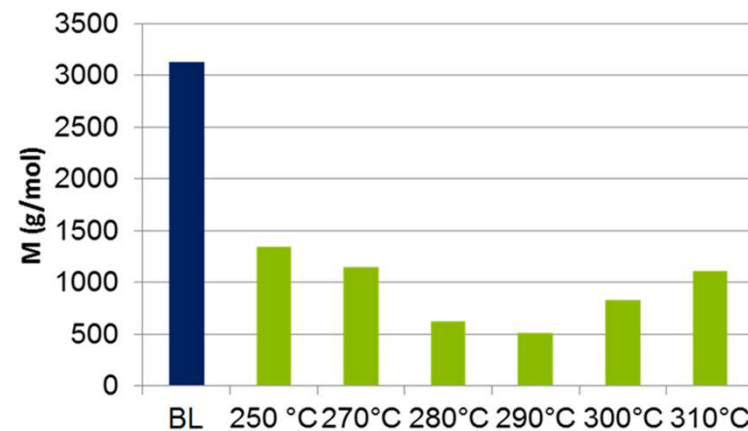


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AQUEOUS PHASE AFTER BLACK LIQUOR CONVERSION



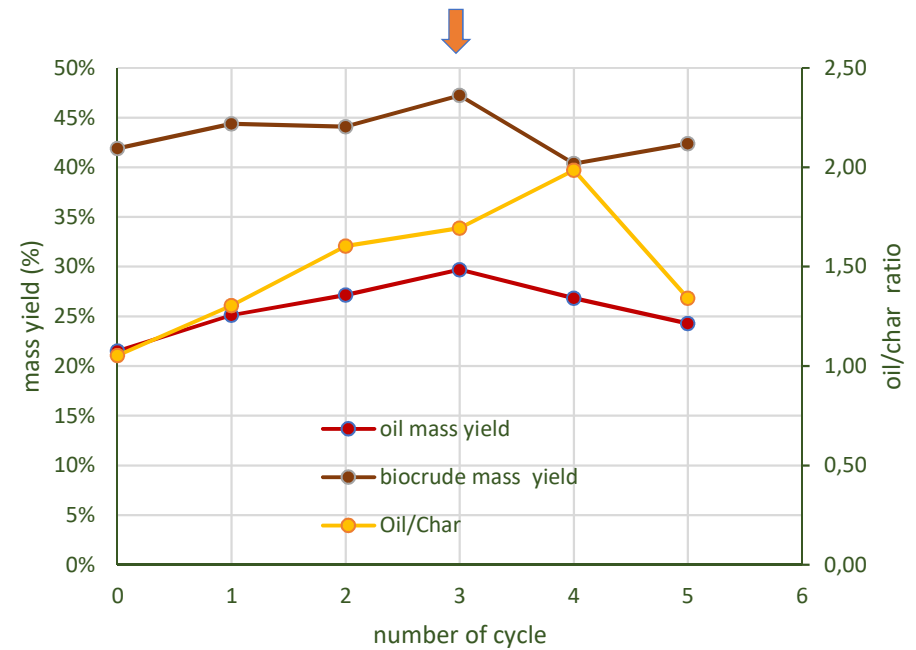
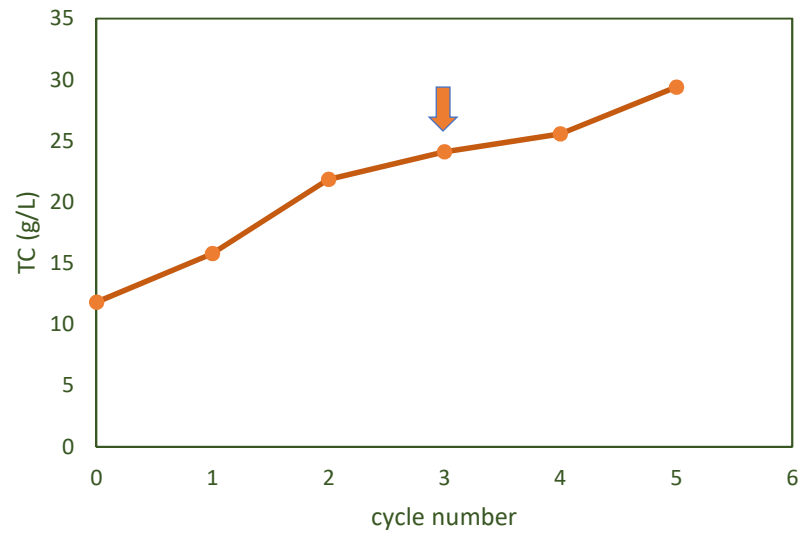
GCMS analyses of residual organic compounds in water (through ethylacetate extraction)



GPC analysis : Mean molecular weight is divided by 6 after hydrothermal treatment (280-290° C)



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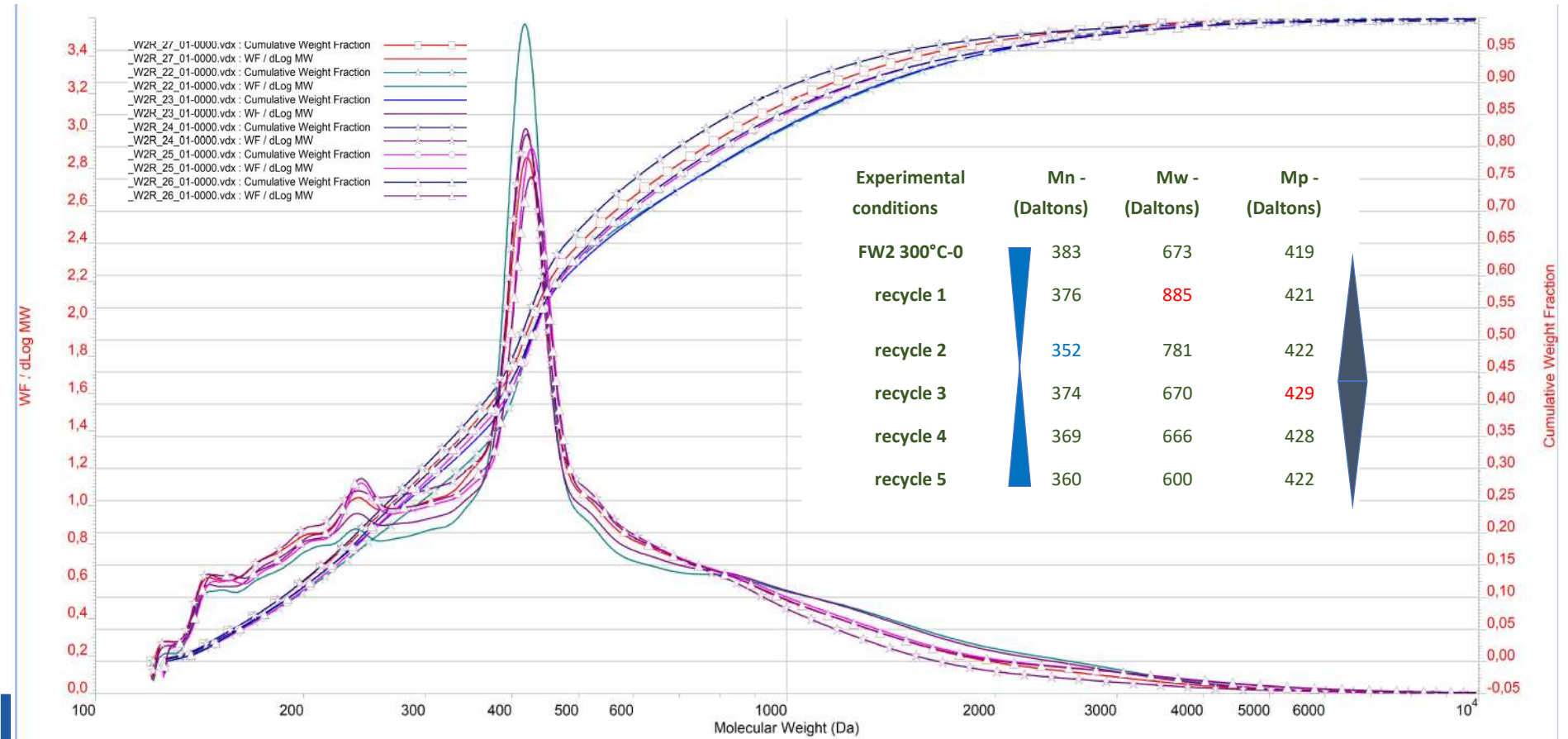


Resource = Food waste 2
Conversion temperature= 300°C

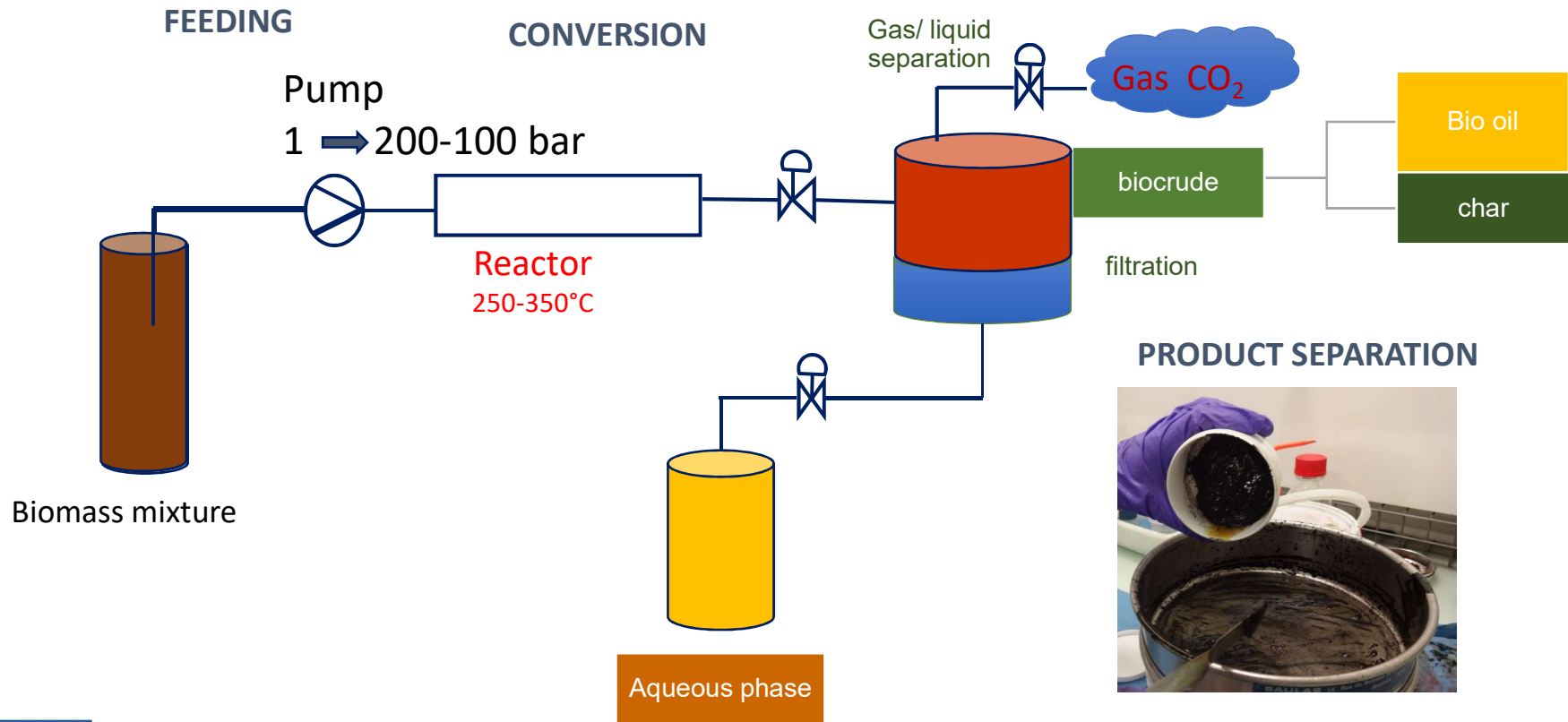


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AQUEOUS PHASE RECYCLING EFFECT

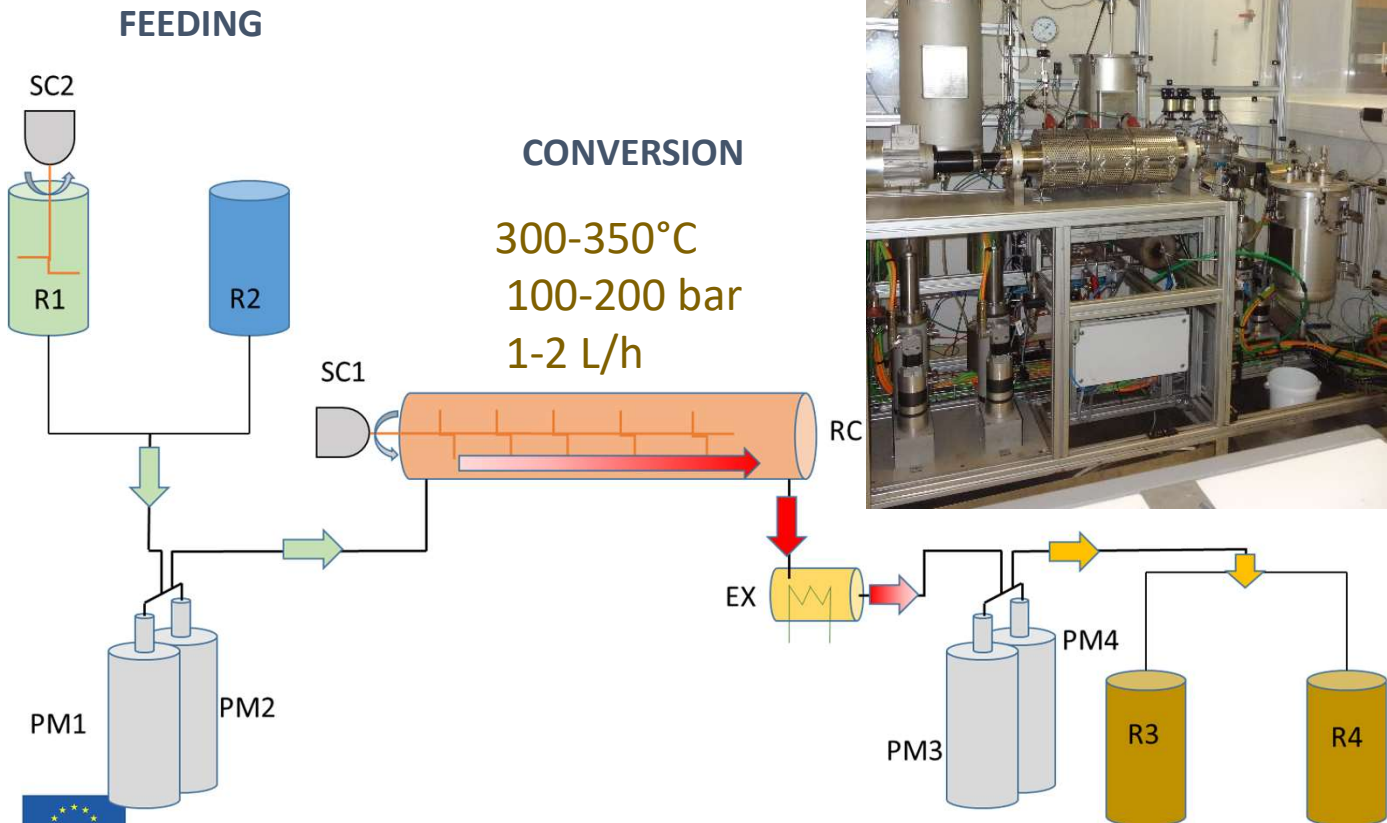


CONTINUOUS PROCESS FLOW CHART



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HTL CONTINUOUS EXPERIMENTAL SET-UP



R1, R2 : water and biomass reservoirs
 PM1, PM2 : feeding pumps
 PM3, PM4 : pressure regulation pumps
 R3, R4 : product recovery reservoirs
 RC : conversion reactor
 EX : heat exchanger
 SC1, SC2 : stirrers



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conversion conditions

300°C

130 bar

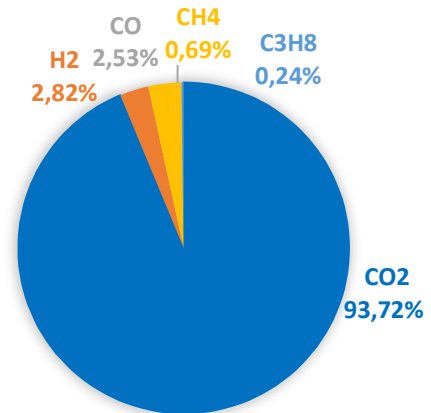
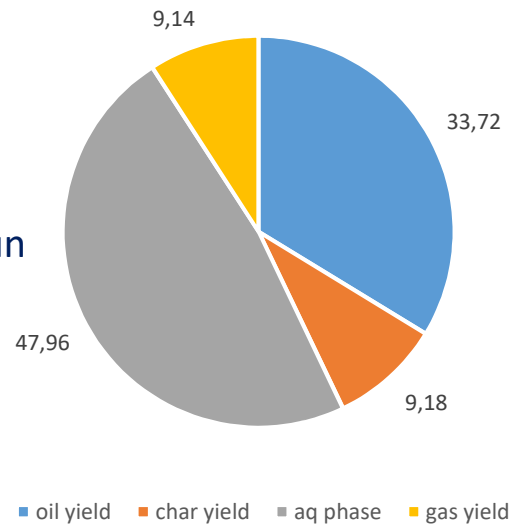
1,5 L/h

RT ~15 min

10 %w of organic matter

Yields in %w

Average of the different run



GAS COMPOSITION % VOL

* Raw Biocrude humidity ~25%



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RESUME of DATA on CONTINUOUS HTL PRODUCTS OF FOOD WASTES

%w	FW dm
C	46,48
H	7,04
N	2,97
S	0,18
ash	5,25
O*	38,09

10% in water

%w	ini aq mixture
C	8,61
H	11,50
N	0,48
S	0,12
pH	4,39

300°C
130 bar
1,5 L/h
RT ~15 min
10 %w of organic matter



%w	biocrude dist
C	74,41
H	10,09
N	2,32
S	0,26
ash	1,50
O*	11,57



%w	aq phase
C	3,26
H	9,90
N	0,28
S	0,23
pH	4,07

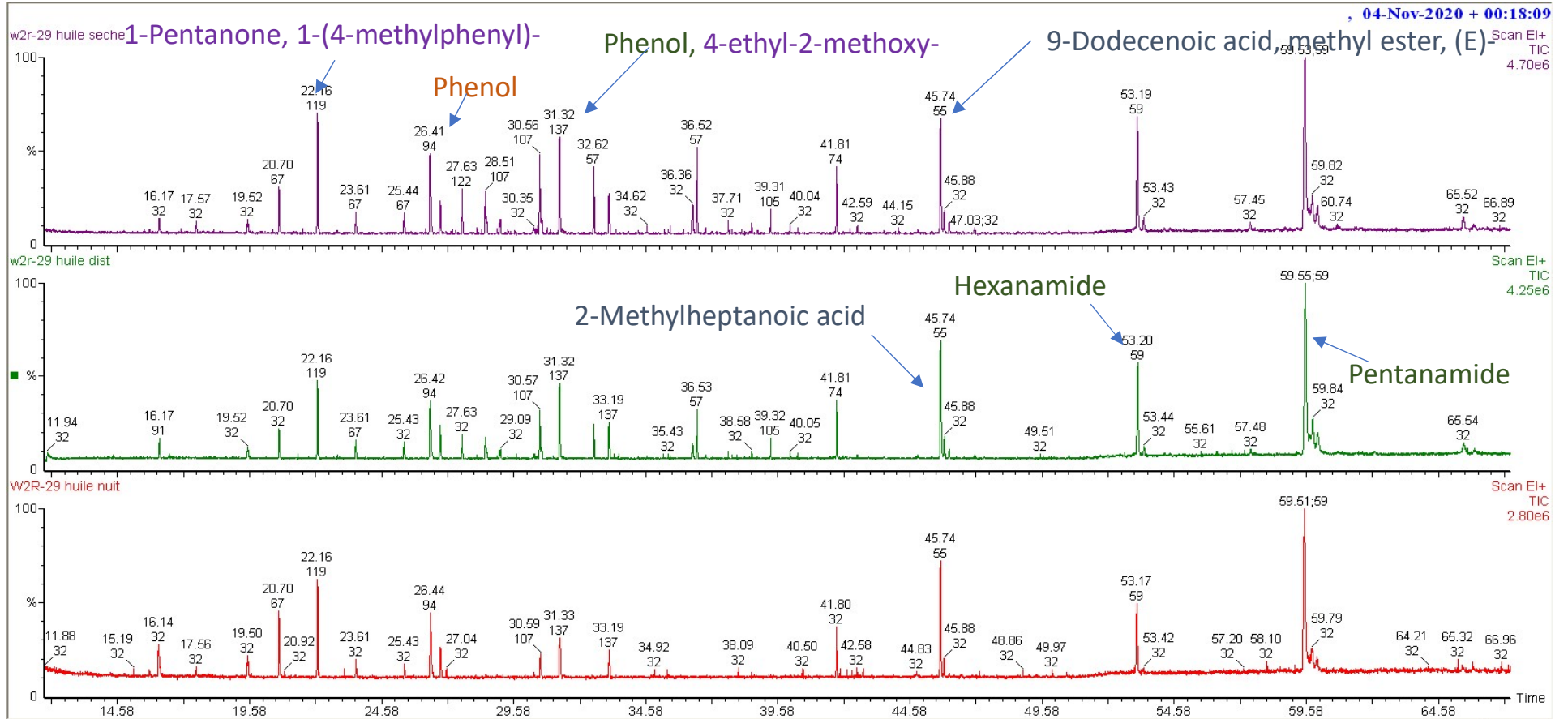
%w	char
C	64,29
H	5,77
N	4,55
S	0,33
O+ash	25,06



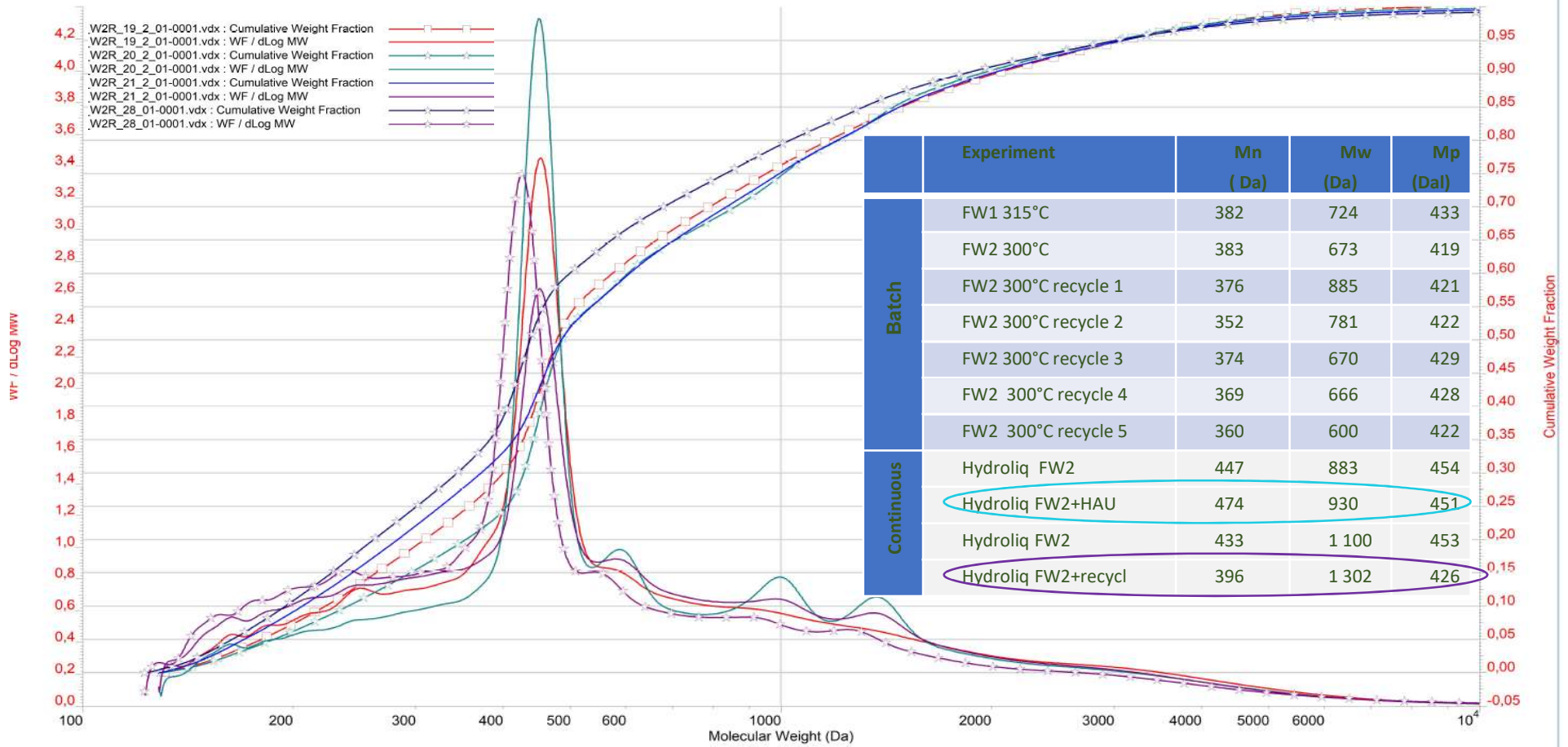
%w	oil
C	77,17
H	11,26
N	1,72
S	0,23
O+ash	9,62



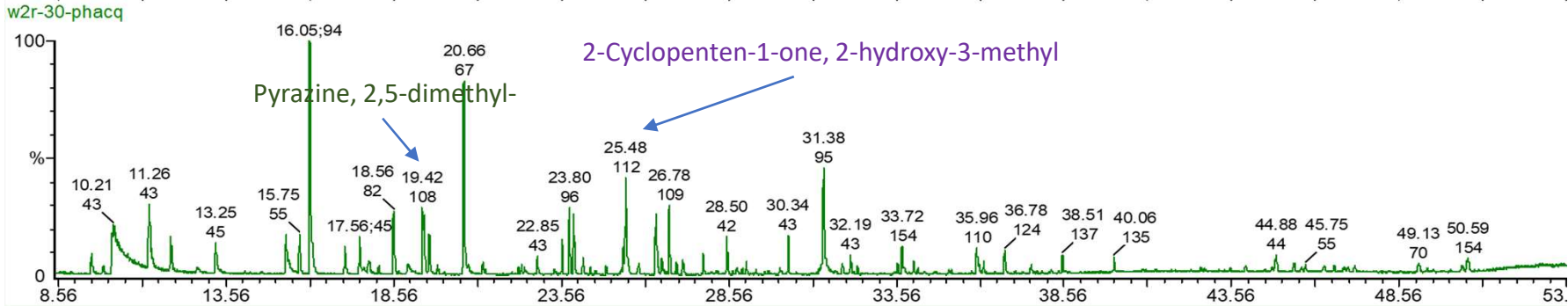
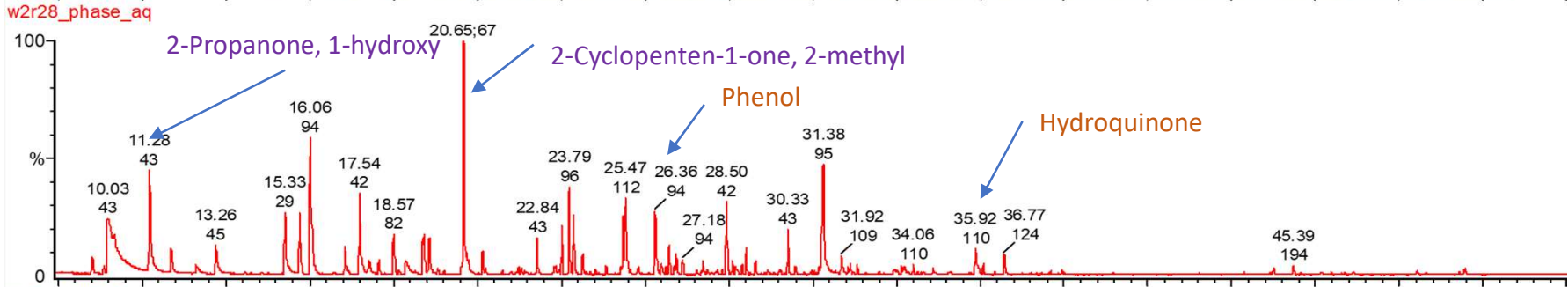
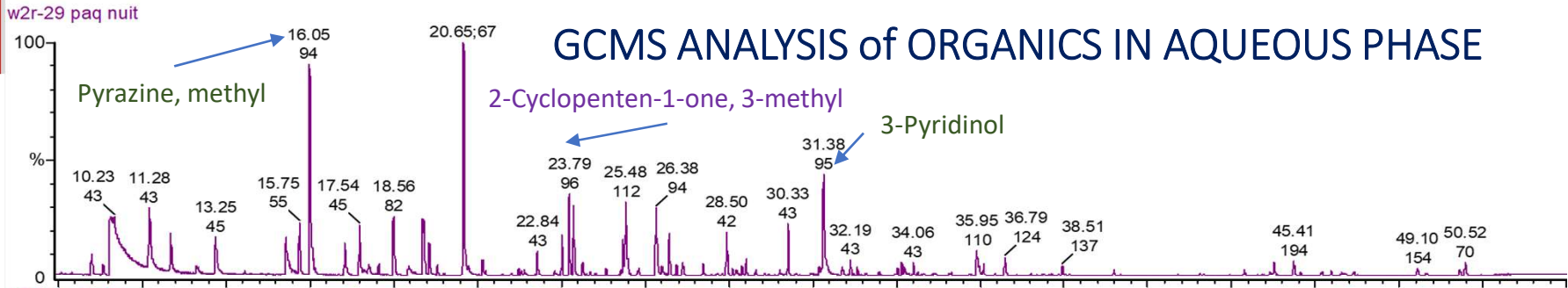
IDENTIFICATION OF MAIN SPECIES BY GCMS in the OIL



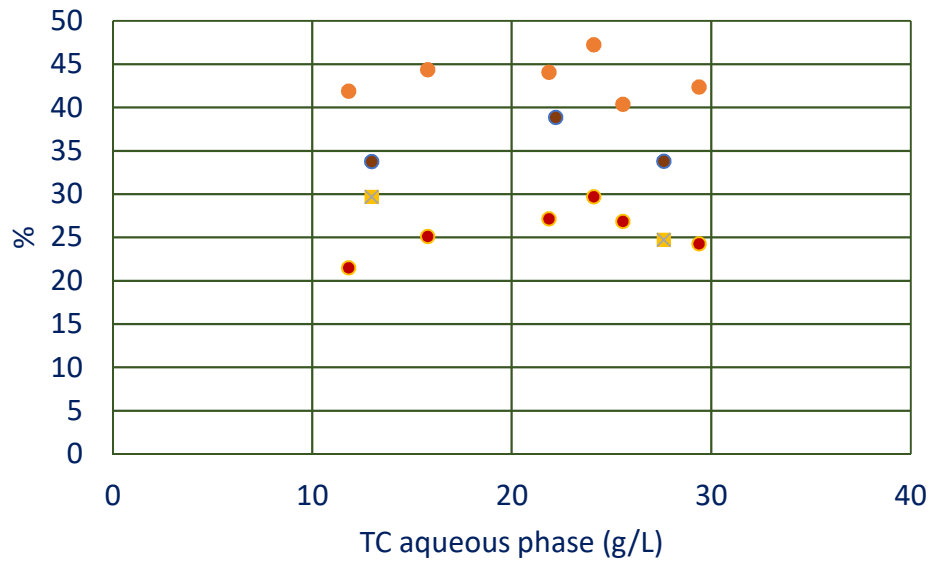
MOLECULAR WEIGHT DISTRIBUTION OF SPECIES in the OIL



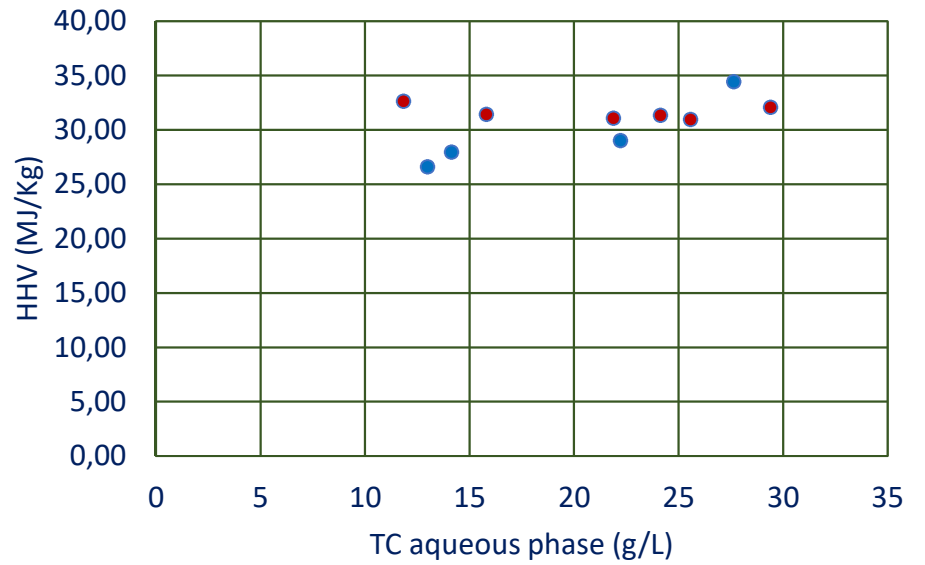
GCMS ANALYSIS of ORGANICS IN AQUEOUS PHASE



BATCH / CONTINUOUS



- biocrude yields continuous ● biocrude yields batch
- biooil yields continuous ● biooil yields batch



- batch ● continuous

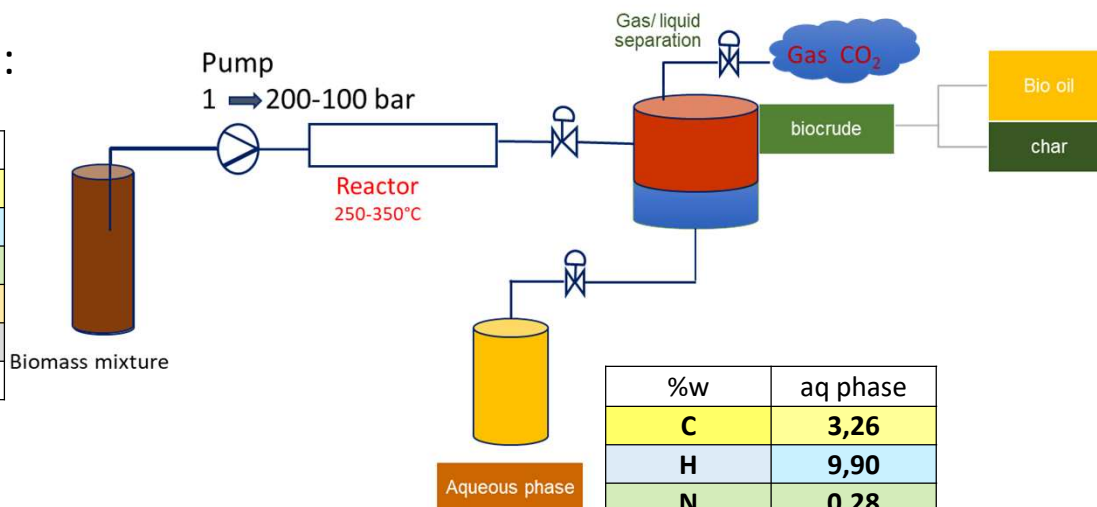


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For food wastes :

%w	FW dm
C	46,48
H	7,04
N	2,97
S	0,18
ash	5,25
O*	38,09

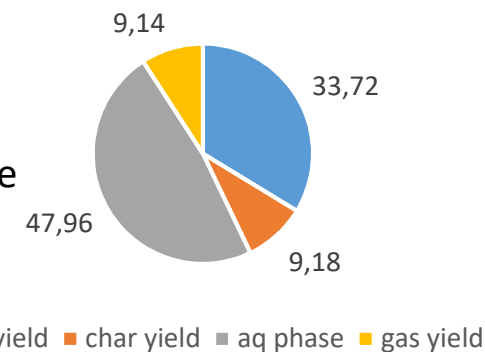
10% in water



%w	aq phase
C	3,26
H	9,90
N	0,28
S	0,23
pH	4,07

%w	oil
C	77,17
H	11,26
N	1,72
S	0,23
O+ash	9,62

%w	char
C	64,29
H	5,77
N	4,55
S	0,33
O+ash	25,06



Challenges :

- Conversion of lignin rich resource
- conversion of resources with high content of inorganics i.e. non reactive matters and abrasive matter (glass, stones ...)
- Reduction of N and O content by upgrading
- Viscosity of biocrude



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WASTE2ROAD 

Any question ?

With contributions of :

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