

Calcium looping for CO₂ capture in cement plants — pilot scale test

Matthias Hornberger*, Reinhold Spörl, Günter Scheffknecht

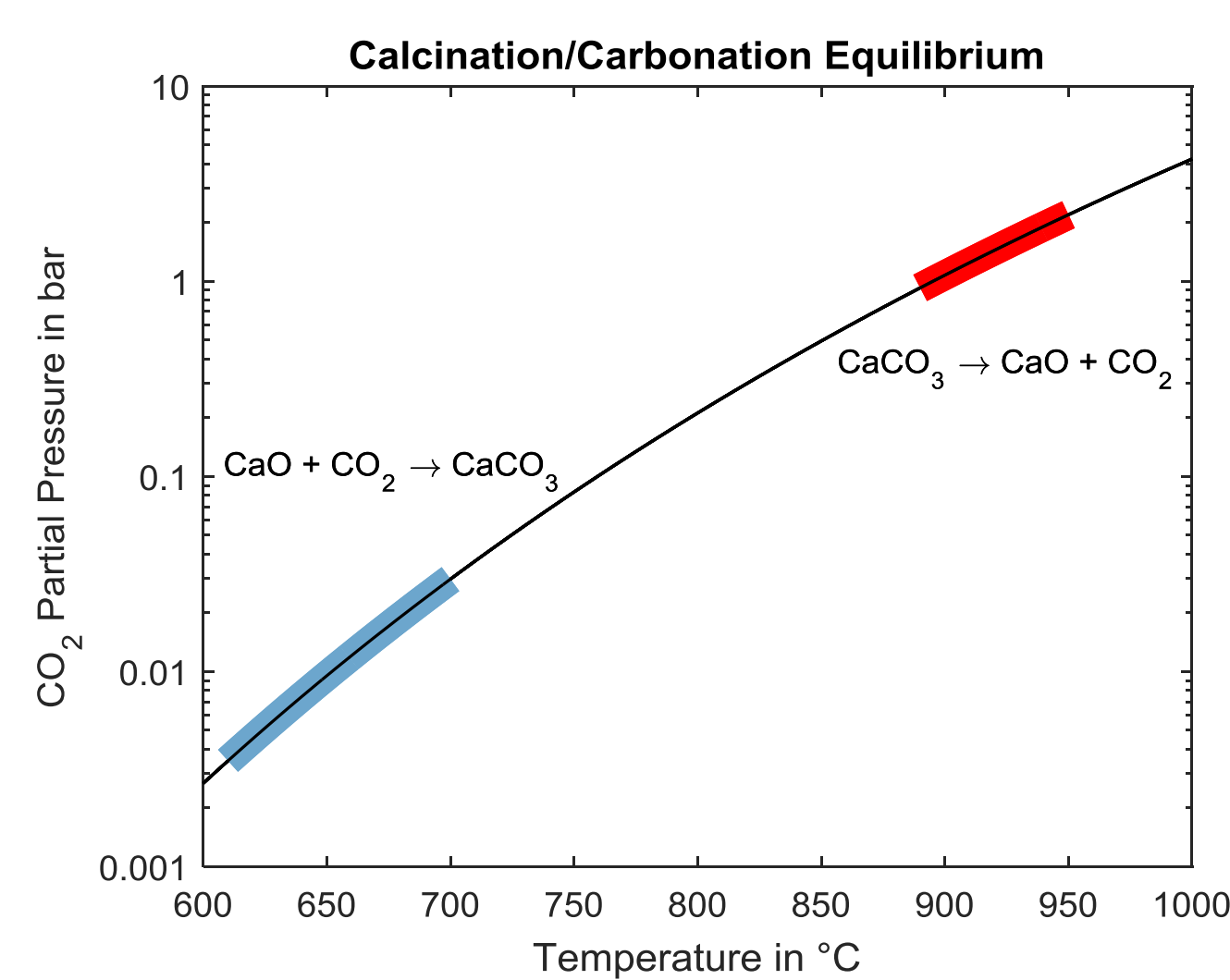
Introduction

- Cement industry is responsible for approx. 5% of global anthropogenic CO₂ emissions
- CCS/CCU technologies shall reduce CO₂ emissions to mitigate climate change
- Calcium looping is a promising post combustion CCS technology for cement industry

Calcium Looping

- Calcium looping is based on the cyclic calcination and carbonation of CaCO₃
- Oxy-fuel calcination leads to CO₂-rich exhaust stream ready for sequestration or utilization
- Supply of high quality energy suitable for efficient power generation or heat integration
- Low CO₂ avoiding costs due to energy integration
- Spent calcium looping sorbent can be (re)utilized in the cement process reducing its original CO₂ flue gas concentration

Calcium Looping Operation Conditions

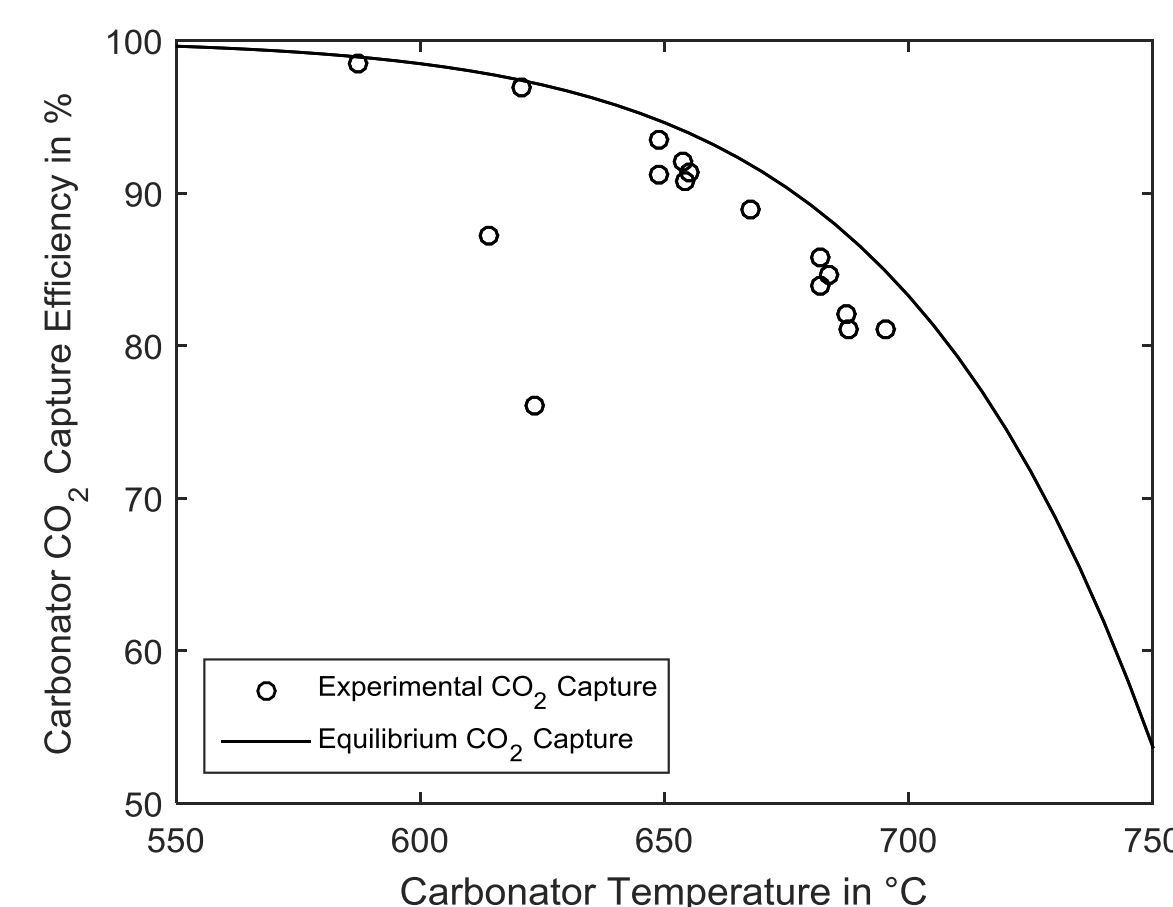


- Oxy-fuel calcination of CaCO₃ requires temperatures around 900 °C
- Compromise between reaction kinetics and equilibrium partial pressure leads to carbonation temperature around 650 °C
- Efficient recuperation of required heat due to high temperature level
- High specific amount of fresh sorbent due to utilization in cement production

Results

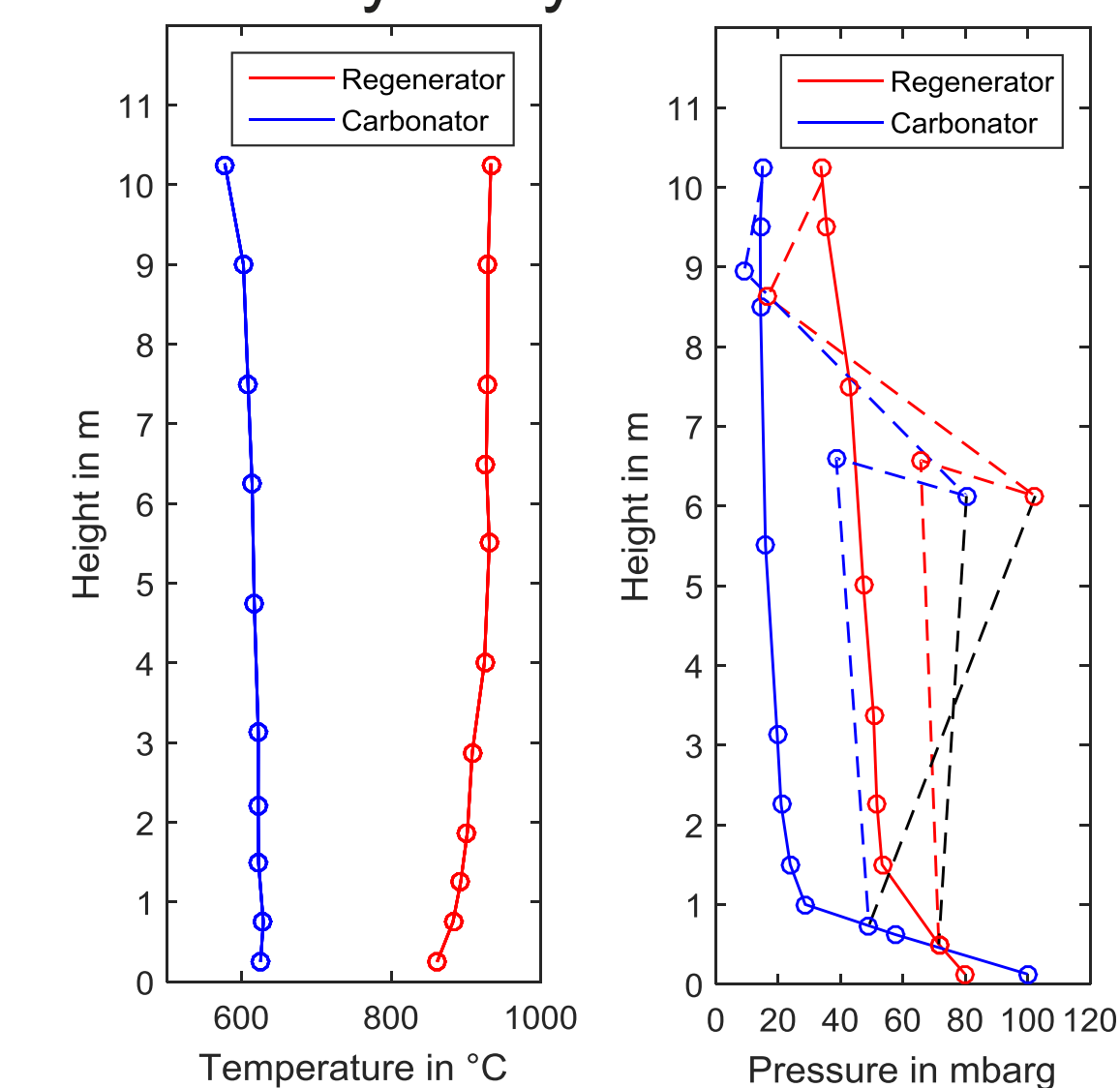
CO₂ capture performance

- CO₂ capture rates above 90 % for carbonator temperature below 650 °C and sufficient space time / looping ratio
- CO₂ capture rates near equilibrium capture rates achieved



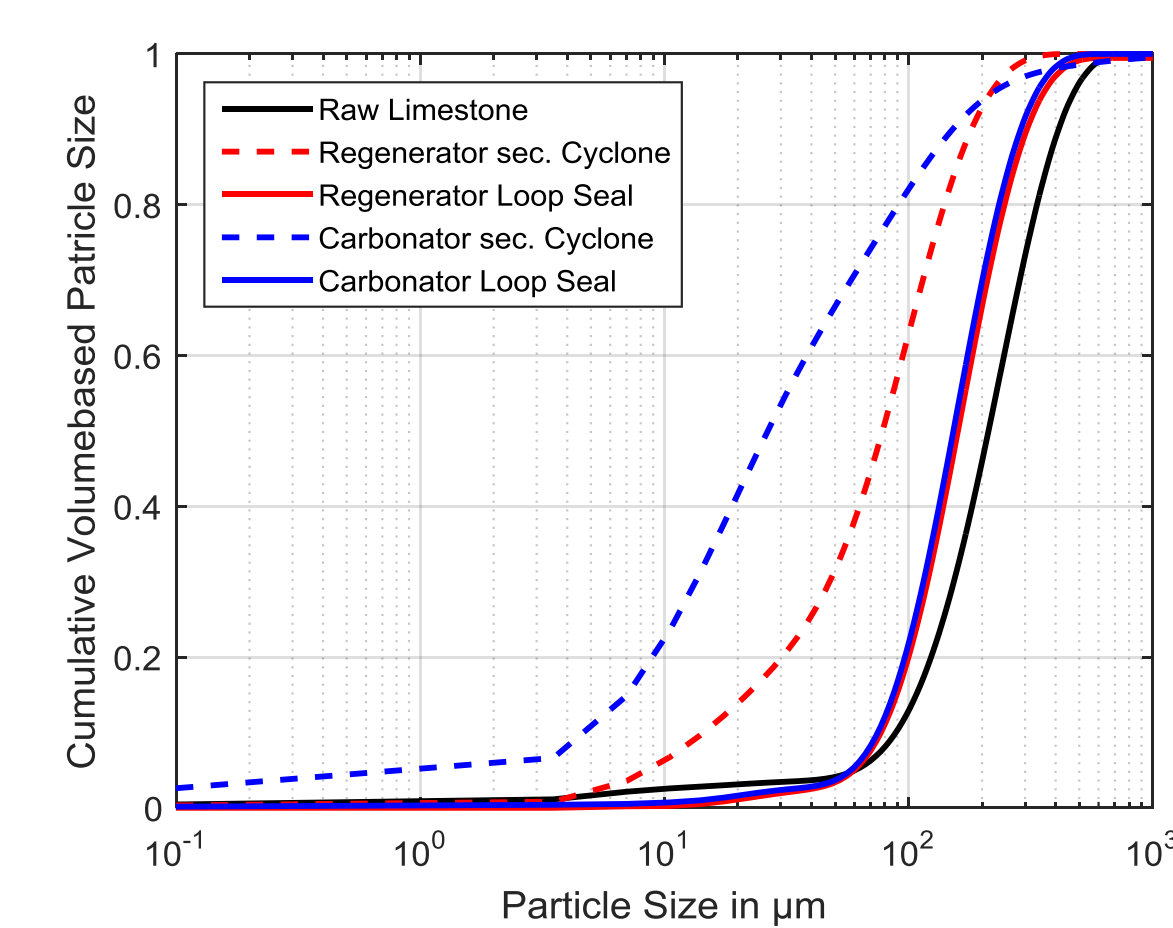
Temperature and hydrodynamic profiles

- Isothermal temperature profiles
- Stable hydrodynamics



Particle size

- Reduced particle size due to attrition

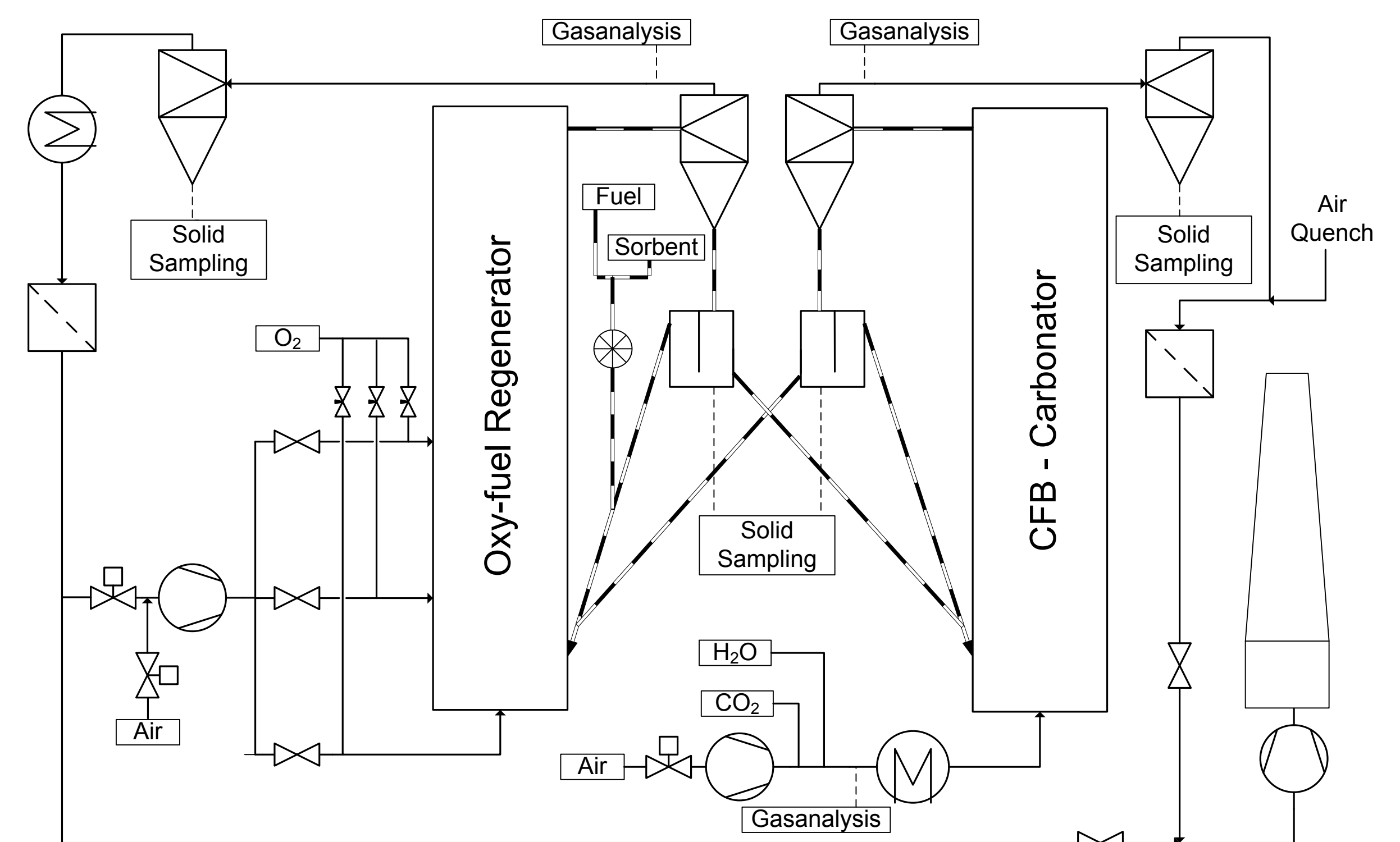


Summary and Discussion

- Investigation of calcium looping process highly integrated into a cement plant resulting in CO₂ flue gas concentration of 15 % and high makeup ratios
- Stable operation was achieved, yielding high CO₂ capture rates (> 90 % over wide parameter range)
- Uniform reaction condition in calciner and carbonator due to isothermal reactor temperature
- High CO₂ concentration in regenerator exhaust stream

Experimental Setup

CFB-CFB configuration of 200 kW_{th} pilot plant (IFK, University of Stuttgart)



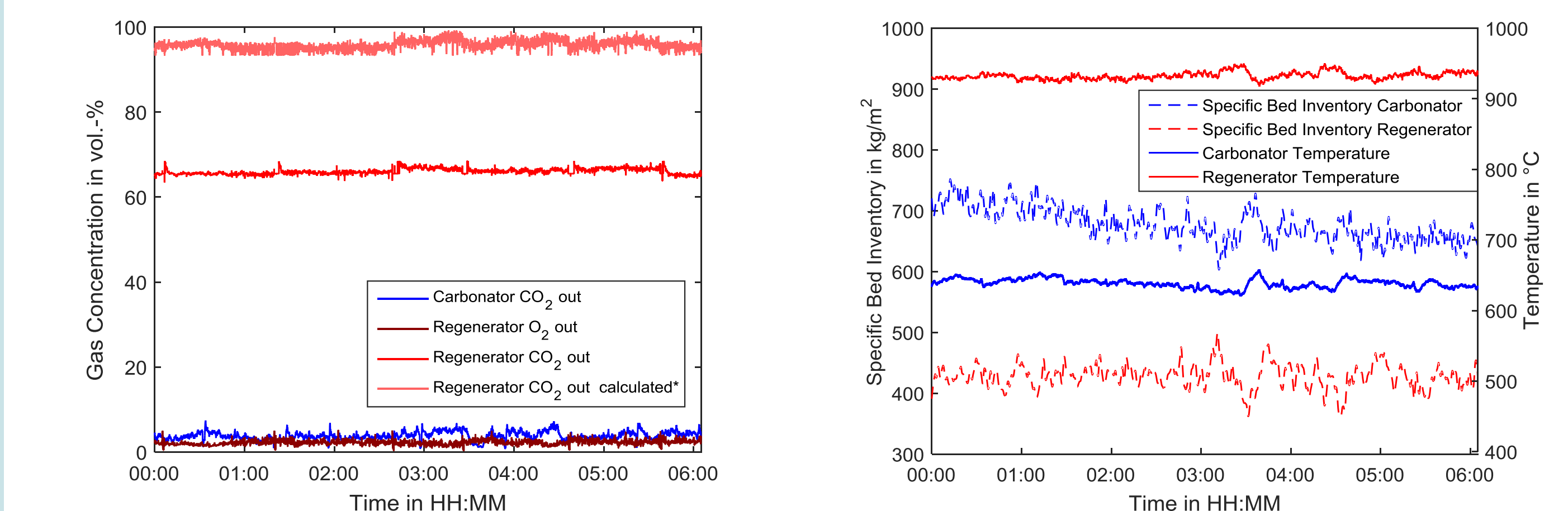
- Refractory lined interconnected circulating fluidized bed reactors (h = 10 m, d_i = 20 cm)
- Oxy-fuel calcination with recycled flue gas (wet)
- Synthetic flue gas mixture (CO₂, H₂O, air) is fed to the carbonator
- Transfer flow controlled by cone valves
- Online gas measurement: CO₂, CO, NO, NO₂, SO₂, H₂, H₂O

Experimental Conditions

- Calcination temperature: T_{Calc} = 890 ... 930 °C
- Carbonation temperature: T_{Carb} = 600 ... 700 °C
- Space time: N_{Ca} / N_{CO2} = 1.2 ... 2 h
- Makeup Ratio: N_{Ca,0} / N_{CO2} = 0.5 ... 0.8
- Looping Ratio: N_{Ca} / N_{CO2} = 7 ... 19
- At least 1 h of steady state operation for each experimental point
- Sorbent analysis by TGA as well as major and trace elementary analysis
- CO₂ flue gas concentration 15 % - assuming cement plants raw meal is completely calcined in calcium looping

Process Demonstration

6 h extract of stable operation during 120 h experimental campaign



^{*)} calculated assuming measurement ports are purged with recycled flue gas and exhaust gas is dried

Outlook

- Investigation of lower integrated calcium looping options resulting in
 - CO₂ concentrations up to 35 %
 - lower makeup ratios
- Measurement of impurities (N₂O, NO_x, etc.) in regenerator relevant for CO₂ compression



Acknowledgements

This project has received funding from the *European Union's Horizon 2020 research and innovation programme* under grant agreement No 641185.

Disclaimer: The European Commission support for the production of this publication does not constitute endorsement of the contents which reflects the views only of the authors, and the Commission cannot be held responsible for any use which may be made of the information contained therein

